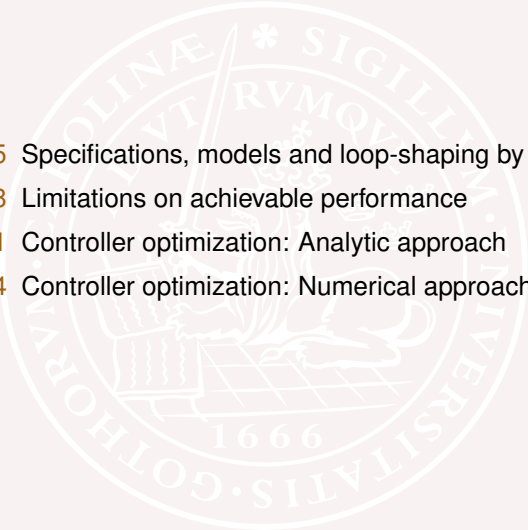# FRTN10 Multivariable Control, Lecture 15

Automatic Control LTH, 2016

Lecture 15: Course Summary

L1-L5   Specifications, models and loop-shaping by hand

L6-L8   Limitations on achievable performance

L9-L11   Controller optimization: Analytic approach

L12-L14   Controller optimization: Numerical approach

Flexible servo resonant system

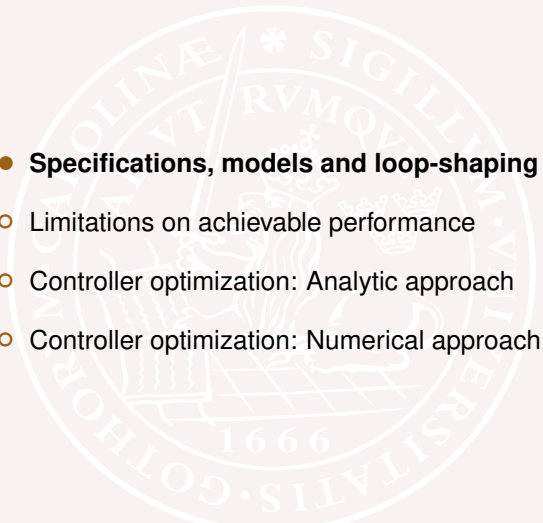Quadruple tank system multivariable (MIMO), NMP zero

Rotating crane multivariable, observer needed

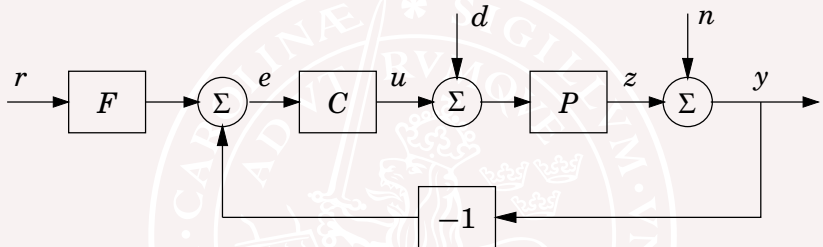DVD control resonant system, wide frequency range, (midranging)

Bicycle steering unstable pole/zero-pair

Distillation column MIMO, input-output pairing

Course Summary

- **Specifications, models and loop-shaping**

- Limitations on achievable performance

- Controller optimization: Analytic approach

- Controller optimization: Numerical approach

2-DOF control

- Reduce the effects of load disturbances
- Limit the effects of measurement noise
- Reduce sensitivity to process variations
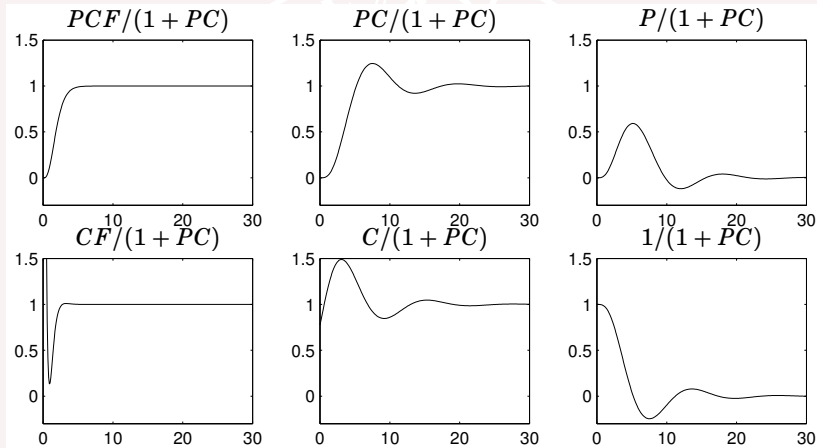- Make output follow command signals
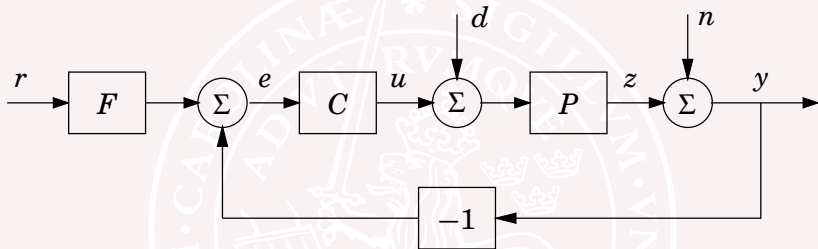
$$U = -\frac{PC}{1+PC}D - \frac{C}{1+PC}N + \frac{CF}{1+PC}R$$

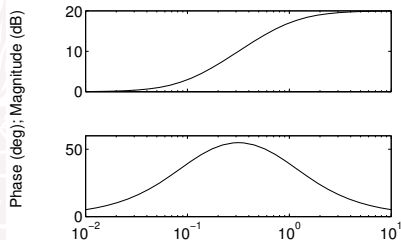$$Y = \frac{P}{1+PC}D + \frac{1}{1+PC}N + \frac{PCF}{1+PC}R$$

Important step responses

$$C(s) = \frac{s + 10}{s + 1} \qquad C(s) = \frac{10(s + 1)}{(s + 10)}$$
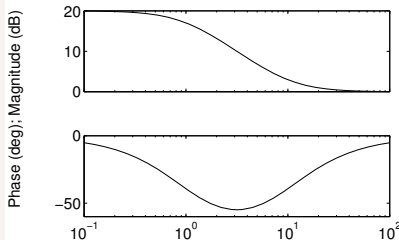
MIMO systems

If C, P and F are general MIMO-systems, so called **transfer function matrices**, the **order of multiplication matters** and

$$PC \neq CP$$

and thus we need to multiply with the inverse from the correct side as in general

$$(I + L)^{-1}M \neq M(I + L)^{-1}$$

Note, however that

$$(I + PC)^{-1}PC = P(I + CP)^{-1}C = PC(I + PC)^{-1}$$

Different gains in different directions:
$$\begin{bmatrix} y_1 \\ y_2 \end{bmatrix} = \begin{bmatrix} 2 & 4 \\ 0 & 3 \end{bmatrix} \begin{bmatrix} u_1 \\ u_2 \end{bmatrix}$$
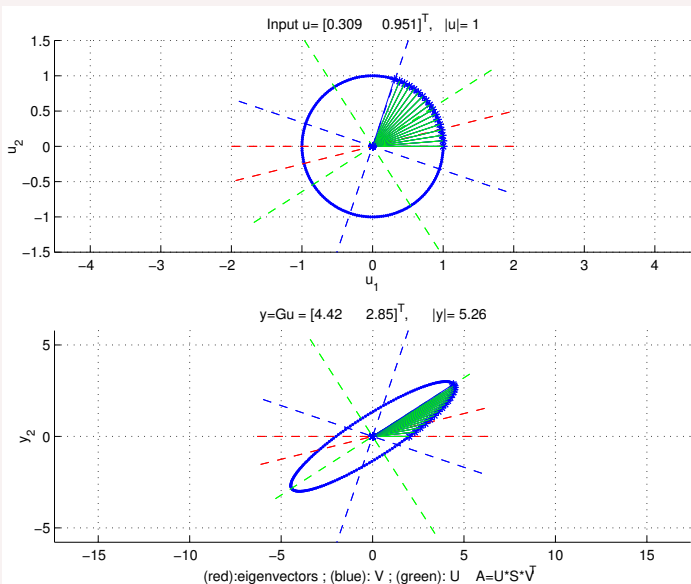
Plot singular values of $G(i\omega)$ versus frequency

» s=tf('s')
» G=[1/(s+1) 1 ; 2/(s+2) 1]
» sigma(G) % plot singular values

% Alt. for a certain frequency:
» w = 1;
» A = [1/(i*w+1) 1; 2/(i*w+2) 1]
» [U,S,V] = svd(A)

Singular Values

Realization of multi-variable system
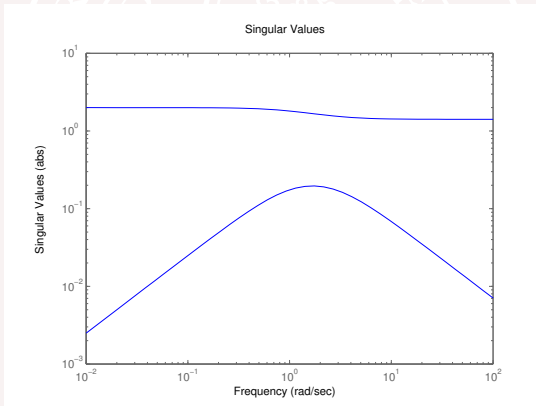
Example: To find state space realization for the system

$$G(s) = \begin{bmatrix} \frac{1}{s+1} & \frac{2}{(s+1)(s+3)} \\ \frac{6}{(s+2)(s+4)} & \frac{1}{s+2} \end{bmatrix}$$

we write the transfer matrix as

$$\begin{bmatrix} \frac{1}{s+1} & \frac{1}{s+1} - \frac{1}{s+3} \\ \frac{3}{s+2} - \frac{3}{s+4} & \frac{1}{s+2} \end{bmatrix} = \frac{\begin{bmatrix} 1 \\ 0 \end{bmatrix} \begin{bmatrix} 1 & 1 \end{bmatrix}}{s+1} + \frac{\begin{bmatrix} 0 \\ 1 \end{bmatrix} \begin{bmatrix} 3 & 1 \end{bmatrix}}{s+2} - \frac{\begin{bmatrix} 1 \\ 0 \end{bmatrix} \begin{bmatrix} 0 & 1 \end{bmatrix}}{s+3} - \frac{\begin{bmatrix} 0 \\ 1 \end{bmatrix} \begin{bmatrix} 3 & 0 \end{bmatrix}}{s+4}$$

This gives the realization

$$\begin{bmatrix} \dot{x}_1(t) \\ \dot{x}_2(t) \\ \dot{x}_3(t) \\ \dot{x}_4(t) \end{bmatrix} = \begin{bmatrix} -1 & 0 & 0 & 0 \\ 0 & -2 & 0 & 0 \\ 0 & 0 & -3 & 0 \\ 0 & 0 & 0 & -4 \end{bmatrix} \begin{bmatrix} x_1(t) \\ x_2(t) \\ x_3(t) \\ x_4(t) \end{bmatrix} + \begin{bmatrix} 1 & 1 \\ 3 & 1 \\ 0 & -1 \\ -3 & 0 \end{bmatrix} \begin{bmatrix} u_1(t) \\ u_2(t) \end{bmatrix}$$

$$\begin{bmatrix} y_1(t) \\ y_2(t) \end{bmatrix} = \begin{bmatrix} 1 & 0 & 1 & 0 \\ 0 & 1 & 0 & 1 \end{bmatrix} x(t)$$

The Small Gain Theorem

Consider a linear system $\mathcal{S}$ with input u and output $\mathcal{S}(u)$ having a (Hurwitz) stable transfer function $G(s)$. Then, the system gain

$$\|\mathcal{S}\| := \sup_u \frac{\|\mathcal{S}(u)\|}{\|u\|} \quad \text{is equal to} \quad \|G\|_\infty := \sup_\omega |G(i\omega)|$$
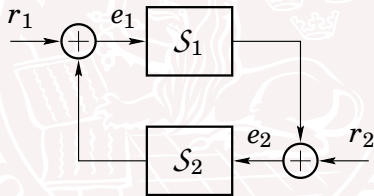
Assume that $\mathcal{S}_1$ and $\mathcal{S}_2$ are input-output stable. If $\|\mathcal{S}_1\| \cdot \|\mathcal{S}_2\| < 1$, then the gain from (r_1, r_2) to (e_1, e_2) in the closed-loop system is finite.
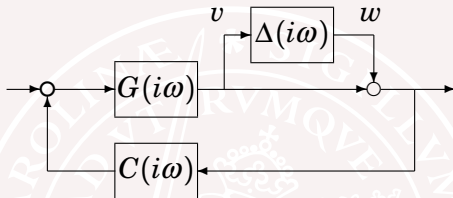
The transfer function from w to v is

$$\frac{G(i\omega)C(i\omega)}{1 + G(i\omega)C(i\omega)}$$

Hence the small gain theorem guarantees closed-loop stability for all perturbations Δ with

$$\|\Delta\| < \left(\sup_\omega \left| \frac{G(i\omega)C(i\omega)}{1 + G(i\omega)C(i\omega)} \right| \right)^{-1}$$
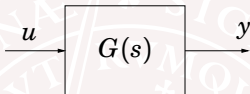
Assume that the stationary mean-zero stochastic process u has spectral density $\Phi_u(\omega)$. Then

$$\Phi_y(\omega) = G(i\omega)\Phi_u(\omega)G(i\omega)^*$$

- "Any spectrum" can be generated by filtering white noise
- Finding $G(s)$ given $\Phi_y(\omega)$ is called spectral factorization

Given the system

$$\dot{x} = Ax + Bv, \qquad \Phi_v(\omega) = R$$
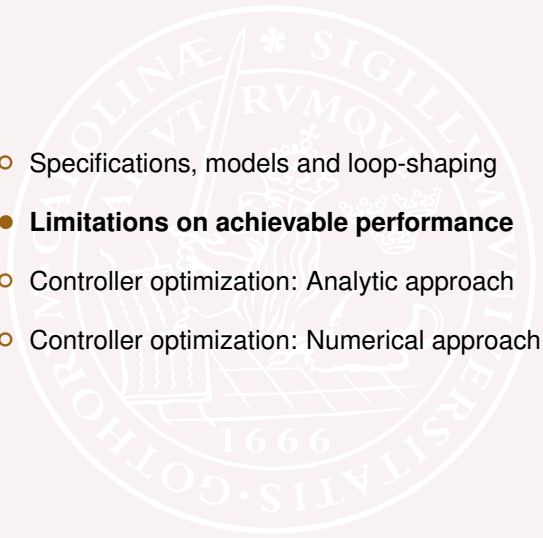
the stationary covariance of the state x is given by

$$\Pi_x = \frac{1}{2\pi} \int_{-\infty}^{\infty} \Phi_x(\omega) d\omega$$

The symmetric matrix Π_x can be found by solving the Lyapunov equation

$$A\Pi_x + \Pi_x A^T + BRB^T = 0$$

Course Summary

○ Specifications, models and loop-shaping

● **Limitations on achievable performance**

○ Controller optimization: Analytic approach

○ Controller optimization: Numerical approach

Example from Lecture 6:
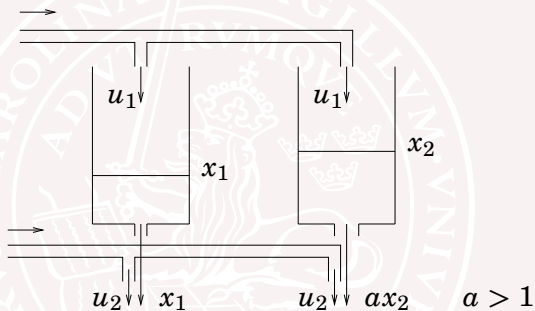
$$\dot{x}_1 = -x_1 + u_1 \qquad\qquad \dot{x}_2 = -ax_2 + u_1$$
$$y_1 = x_1 + u_2 \qquad\qquad y_2 = ax_2 + u_2$$

Can you reach $y_1 = 1, y_2 = 2$?   Can you stay there?

Example: Two water tanks

$$\dot{x}_1 = -x_1 + u_1 \qquad\qquad \dot{x}_2 = -ax_2 + u_1$$
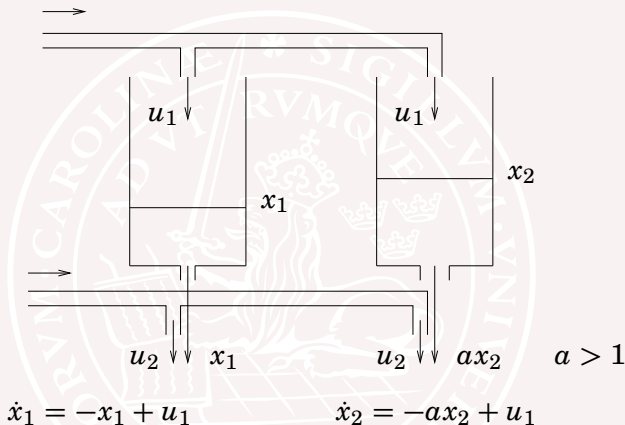
The controllability Gramian $S = \int_0^\infty \begin{bmatrix} e^{-t} \\ e^{-at} \end{bmatrix} \begin{bmatrix} e^{-t} \\ e^{-at} \end{bmatrix}^T dt = \begin{bmatrix} \frac{1}{2} & \frac{1}{a+1} \\ \frac{1}{a+1} & \frac{1}{2a} \end{bmatrix}$

is close to singular for $a \approx 1$, so it is harder to reach a desired state.

Computing the controllability Gramian

The controllability Gramian $S = \int_0^\infty e^{At} B B^T e^{A^T t} dt$ can be computed by solving the linear system of equations

$$AS + SA^T + BB^T = 0$$

$S = S^T > 0$, i.e., S is a symmetric positive definite matrix

Example: For a 2-state system, assign

$$S = \begin{bmatrix} s_{11} & s_{12} \\ s_{12} & s_{22} \end{bmatrix}$$

Multiply together and solve for s_{11}, s_{12}, s_{22} in the same way as you also do for the spectral factorization and the Riccati equations...

Example: Two water tanks
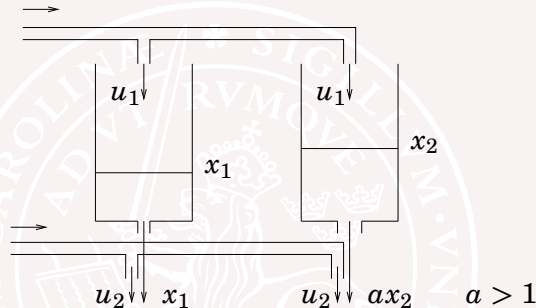
$$\dot{x}_1 = -x_1 + u_1 \qquad \dot{x}_2 = -ax_2 + u_1$$

$$G(s) = \begin{bmatrix} \frac{1}{s+1} & 1 \\ \frac{2}{s+2} & 1 \end{bmatrix}. \quad \text{Find zero from} \quad \det G(s) = \frac{-s}{(s+1)(s+2)}$$

There is a zero at $s = 0$! Outputs must be equal at stationarity.

Sensitivity bounds from RHP zeros and poles

Rules of thumb:

"The closed-loop bandwidth must be less than z."
"The closed-loop bandwidth must be greater than p."
"Time delays T must be less than $1/p$."

Hard bounds:

The sensitivity must be one at an unstable zero:

$$P(z) = 0 \qquad \Rightarrow \qquad S(z) := \frac{1}{1 + P(z)C(z)} = 1$$

The complimentary sensitivity must be one at an unstable pole:

$$P(p) = \infty \qquad \Rightarrow \qquad T(p) := \frac{P(p)C(p)}{1 + P(p)C(p)} = 1$$

Maximum Modulus Theorem

Assume that $G(s)$ is rational, proper and stable. Then

$$\max_{\text{Re } s \geq 0} |G(s)| = \max_{\omega \in \mathbf{R}} |G(i\omega)|$$

Corollary:

Suppose that the plant $P(s)$ has unstable zeros z_i and unstable poles p_j. Then the specifications

$$\sup_{\omega} |W_S(i\omega)S(i\omega)| < 1 \qquad \sup_{\omega} |W_T(i\omega)T(i\omega)| < 1$$

are impossible to meet with a stabilizing controller unless $\|W_S(z_i)\| < 1$ for every unstable zero z_i and $\|W_T(p_j)\| < 1$ for every unstable pole p_j.
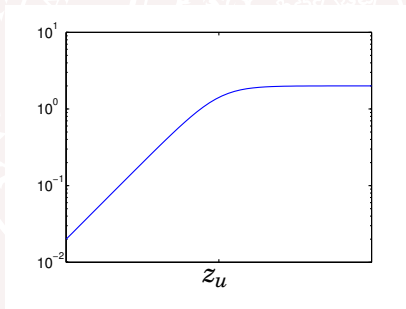
Hard limitations from unstable zeros

If the plant has an unstable zero z_u, then the specification

$$\left| \frac{1}{1 + P(i\omega)C(i\omega)} \right| < \frac{2}{\sqrt{1 + z_u^2/\omega^2}} \qquad \text{for all } \omega$$

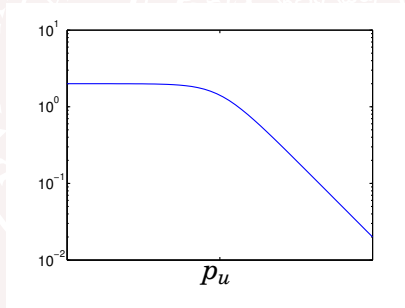is impossible to satisfy.

Examples: Rear-wheel steering and quadruple tank process

Hard limitations from unstable poles

If the plant has an unstable pole p_u, then the specification

$$\left| \frac{P(i\omega)C(i\omega)}{1 + P(i\omega)C(i\omega)} \right| < \frac{2}{\sqrt{\omega^2/p_u^2 + 1}} \qquad \text{for all } \omega$$

is impossible to satisfy.

Example: Inverted pendulum

Nonmin-phase zero and unstable pole

Let $P = \widehat{P}(s-z)(s-p)^{-1}$, with $\widehat{P}$ proper and $\widehat{P}(p) \neq 0$.

Then, for stable closed loop the sensitivity function satisfies

$$\sup_{\omega} |S(i\omega)| \geq \left| \frac{z+p}{z-p} \right|$$

so if $p \approx z$, then the sensitivity function must have a high peak **for every controller** C.

Example: Bicycle with rear wheel steering

$$\frac{\theta(s)}{\delta(s)} = \frac{am\ell V_0}{bJ} \cdot \frac{(-s + V_0/a)}{(s^2 - mg\ell/J)}$$

Relative Gain Array (RGA)

For a square matrix $A \in \mathbf{C}^{n \times n}$, define

$$\mathsf{RGA}(A) := A. * (A^{-1})^T$$

where ".*" denotes element-by-element multiplication.
(For a non-square matrix, use pseudo inverse $A^\dagger$)

- The sum of all elements in a column or row is one.
- Permutations of rows or columns in A give the same permutations in RGA(A)
- $\mathsf{RGA}(A) = \mathsf{RGA}(D_1 A D_2)$ if D_1 and D_2 are diagonal, i.e. RGA(A) is independent of scaling
- If A is triangular, then RGA(A) is the unit matrix I.

- Find a permutation of inputs and outputs that makes RGA($P(0)$) as close as possible to the identity matrix.
- Avoid pairings that give negative diagonal elements of RGA($P(0)$)

$$\text{RGA}(P(0)) = \begin{bmatrix} 0.2827 & -0.6111 & 1.3285 \\ 0.0134 & 1.5827 & -0.5962 \end{bmatrix}$$

To choose control signal for y_1, we apply the heuristics to the top row and choose u_3. Based on the bottom row, we choose u_2 to control y_2. Decentralized control!

Decoupling

Simple idea: Find a compensator so that the system appears to be without coupling ("block-diagonal transfer function matrix").

- Input decoupling $Q = PD_1$
- Output decoupling $Q = D_2P$
- "both" $Q = D_2PD_1$
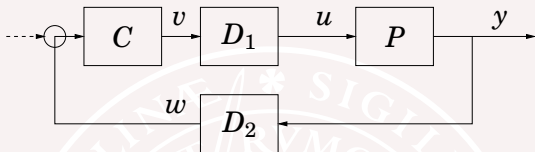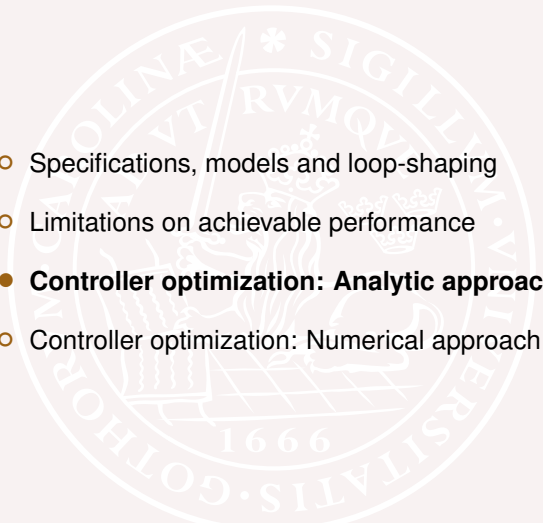
Find D_1 and D_2 so that the controller sees a "diagonal plant":

$$D_2 P D_1 = \begin{bmatrix} * & 0 & 0 \\ 0 & * & 0 \\ 0 & 0 & * \end{bmatrix}$$

Then we can use a "decentralized" controller C with same block-diagonal structure.

Course Summary

o Specifications, models and loop-shaping

o Limitations on achievable performance

● **Controller optimization: Analytic approach**

o Controller optimization: Numerical approach

controlled variables z · distubances w

Plant

measurements y · control inputs u
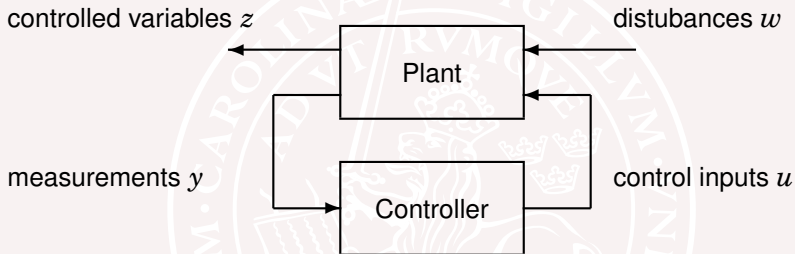
Controller

The objective is to find a controller that optimizes the transfer matrix $G_{zw}(s)$ from disturbances w to controlled outputs z.

Lecture 9-11: Problems with analytic solutions
Lectures 12-14: Problems with numeric solutions

Output feedback using state estimates
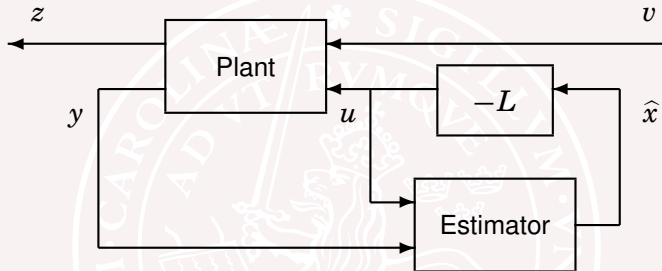
Plant:
$$\begin{cases} \dot{x}(t) = Ax(t) + Bu(t) + v_1(t) \\ y(t) = Cx(t) + v_2(t) \end{cases}$$

Controller:
$$\begin{cases} \frac{d}{dt}\widehat{x}(t) = A\widehat{x}(t) + Bu(t) + K[y(t) - C\widehat{x}(t)] \\ u(t) = -L\widehat{x}(t) \end{cases}$$

Linear Quadratic Gaussian (LQG) control

Given the linear plant

$$\begin{cases} \dot{x}(t) = Ax(t) + Bu(t) + v_1(k) \\ y(t) = Cx(t) + v_2(t) \end{cases} \qquad Q = \begin{bmatrix} Q_1 & Q_{12} \\ Q_{12}^T & Q_2 \end{bmatrix} > 0$$

$$R = \begin{bmatrix} R_1 & R_{12} \\ R_{12}^T & R_2 \end{bmatrix} > 0$$

consider controllers of the form $u = -L\widehat{x}$ with
$\frac{d}{dt}\widehat{x} = A\widehat{x} + Bu + K[y - C\widehat{x}]$. The cost function

$$\mathbf{E}\left\{ x^T Q_1 x + 2x^T Q_{12} u + u^T Q_2 u \right\}$$

is minimized when K and L satisfy

$$0 = Q_1 + A^T S + SA - (SB + Q_{12})Q_2^{-1}(SB + Q_{12})^T \qquad L = Q_2^{-1}(SB + Q_{12})^T$$

$$0 = R_1 + AP + PA^T - (PC^T + R_{12})R_2^{-1}(PC^T + R_{12})^T \qquad K = (PC^T + R_{12})R_2^{-1}$$

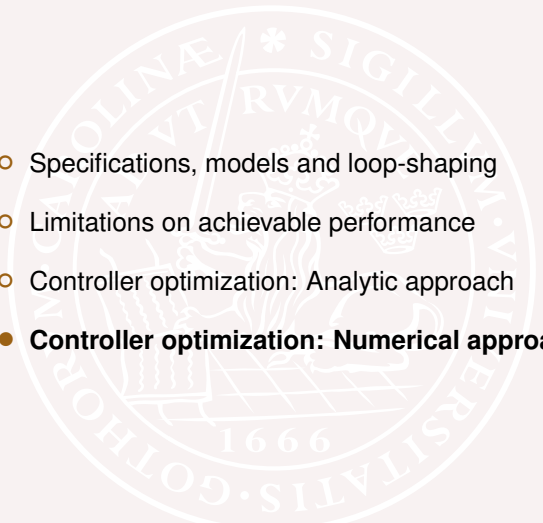The minimal value of the cost is

$$\operatorname{tr}(SR_1) + \operatorname{tr}[PL^T(B^T SB + Q_2)L]$$

Tuning the weights

- A small Q_2 compared to Q_1 means that control is "cheap"
  - Resulting LQ controller will have large feedback gain
  - The plant state will be quickly regulated to zero
  - A large cost on an individual state x_i means that more effort will be spent on regulating that particular state to zero

- A small R_2 compared to R_1 means that measurements can be trusted
  - Resulting Kalman filter will have large filter gain
  - The initial estimation error will quickly converge to zero
  - A large noise covariance on an individual state x_i means that the estimation error will decay faster for that particular state

Course Summary

- Specifications, models and loop-shaping

- Limitations on achievable performance

- Controller optimization: Analytic approach

- **Controller optimization: Numerical approach**

The Q-parameterization (Youla)

controlled variables z distubances w

Plant

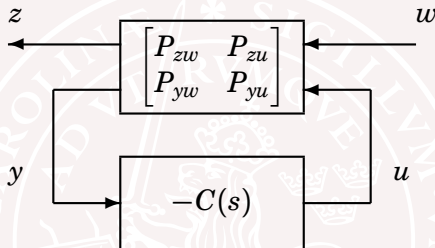measurements y control inputs u
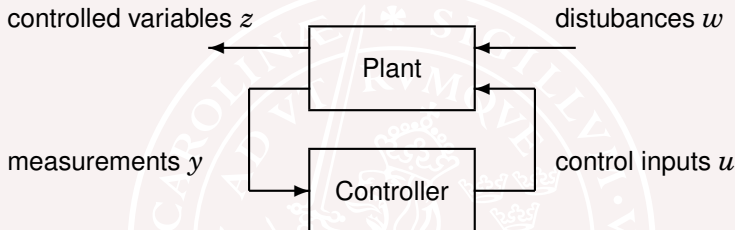
Controller

Idea for lecture 12-14:

The choice of controller generally corresponds to finding $Q(s)$, to get desirable properties of the map from w to z:
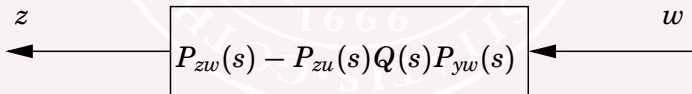
$$z \qquad \boxed{P_{zw}(s) - P_{zu}(s)Q(s)P_{yw}(s)} \qquad w$$

Once $Q(s)$ is determined, a corresponding controller is derived.

The Youla Parameterization

The closed-loop transfer matrix from w to z is

$$G_{zw}(s) = P_{zw}(s) - P_{zu}(s)Q(s)P_{yw}(s)$$

where

$$Q(s) = C(s)\big[I + P_{yu}(s)C(s)\big]^{-1}$$
$$C(s) = Q(s) + Q(s)P_{yu}(s)C(s)$$
$$C(s) = \big[I - Q(s)P_{yu}(s)\big]^{-1}Q(s)$$

Synthesis by convex optimization

A general control synthesis problem can be stated as a convex optimization problem in the variables $Q_0, \ldots, Q_m$. The problem has a quadratic objective, with linear and quadratic constraints:

Minimize $\int_{-\infty}^{\infty} |P_{zw}(i\omega) + P_{zu}(i\omega) \overbrace{\sum_k Q_k \phi_k(i\omega)}^{Q(i\omega)} P_{yw}(i\omega)|^2 d\omega \left.\rule{0cm}{0.8cm}\right\}$ quadratic objective

subject to $\left.\begin{array}{l}\text{step response } w_i \to z_j \text{ is smaller than } f_{ijk} \text{ at time } t_k \\ \text{step response } w_i \to z_j \text{ is bigger than } g_{ijk} \text{ at time } t_k\end{array}\right\}$ linear constraints

$\phantom{\text{subject to}}$ Bode magnitude $w_i \to z_j$ is smaller than h_{ijk} at ω_k $\left.\rule{0cm}{0.4cm}\right\}$ quadratic constraints

Once the variables $Q_0, \ldots, Q_m$ have been optimized, the controller is obtained as $C(s) = \left[I - Q(s)P_{yu}(s)\right]^{-1} Q(s)$

Model reduction by balanced truncation

Consider a balanced realization of a stable system,

$$\begin{bmatrix} \dot{\xi}_1 \\ \dot{\xi}_2 \end{bmatrix} = \begin{bmatrix} A_{11} & A_{12} \\ A_{21} & A_{22} \end{bmatrix} \begin{bmatrix} \xi_1 \\ \xi_2 \end{bmatrix} + \begin{bmatrix} B_1 \\ B_2 \end{bmatrix} u \qquad \Sigma = \begin{bmatrix} \Sigma_1 & 0 \\ 0 & \Sigma_2 \end{bmatrix}$$

$$y = \begin{bmatrix} C_1 & C_2 \end{bmatrix} \begin{bmatrix} \xi_1 \\ \xi_2 \end{bmatrix} + Du$$

with the lower part of the Gramian being $\Sigma_2 = \begin{bmatrix} \sigma_{r+1} & & 0 \\ & \ddots & \\ 0 & & \sigma_n \end{bmatrix}$.

Replacing the second state equation by $\dot{\xi}_2 = 0$ gives the relation
$0 = A_{21}\xi_1 + A_{22}\xi_2 + B_2 u$. The reduced system

$$\begin{cases} \dot{\xi}_1 = (A_{11} - A_{12}A_{22}^{-1}A_{21})\xi_1 + (B_1 - A_{12}A_{22}^{-1}B_2)u \\ y_r = (C_1 - C_2A_{22}^{-1}A_{21})\xi_1 + (D - C_2A_{22}^{-1}B_2)u \end{cases}$$

satisfies the error bound

$$\frac{\|y - y_r\|_2}{\|u\|_2} \leq 2\sigma_{r+1} + \cdots + 2\sigma_n$$