Feedforward Design

Real-Time Systems, Lecture 10

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Lecture 10 – Feedforward Design

[IFAC PB Chapter 9; These slides]

- · Reduction of measurable disturbances by feedforward
- Using feedforward to improve setpoint response
 - The servo problem
 - Reference generation input–output approach
 - Reference generation state-space approach
 - Nonlinear reference generation



Approximate Inverse – Example

Let

$$G(s) = rac{6(1-s)}{(s+2)(s+3)}$$

ZOH sampling with h = 0.1 gives

$$H(z) = \frac{-0.4420(z - 1.106)}{(z - 0.8187)(z - 0.7408)} = \frac{B(z)}{A(z)}$$

 $H^{-1}(z)$ noncausal and unstable. Approximate inverse:

$$B^+(z) = 1$$
, $B^-(z) = -0.4420(z - 1.106)$, $d = 1$

$$H^{\dagger}(z) = \frac{(z - 0.8187)(z - 0.7408)}{-0.4420z(1 - 1.106z)}$$

Using feedforward to improve setpoint response

The servo problem: Make the output respond to setpoint changes in the desired way

Typical design criteria:

- Rise time, T_r
- Overshoot, M
- Settling time, Ts
- Steady-state error, e0
- ...



Simplistic Setpoint Handling – Error Feedback



Potential problems:

- Step changes in the setpoint can introduce very large control signals
- The same controller *H_c*(*z*) must be tuned to handle both disturbances and setpoint changes
 - No separation between the regulator problem and the servo problem

Common Quick Fixes

• Filter the setpoint signal



· Rate-limit the setpoint signal



Introduce setpoint weighting in the controller
E.g. PID controller with setpoint weightings β and γ

A More General Solution

Use a two-degree-of-freedom (2-DOF) controller, e.g.:



Design procedure:

- 1. Design feedback controller *H*_{tb} to get good regulation properties (attenuation of load disturbances and measurement noise)
- 2. Design feedforward compensator $H_{\rm ff}$ to obtain the desired servo performance

Separation of concerns

2-DOF Control Structures

A 2-DOF controller can be represented in many different ways, e.g.:



For linear systems, all these structures are equivalent

Example: PID with Setpoint Weighting

$$u = K \left(\beta y_{sp} - y + \frac{1}{T_I} \int (y_{sp} - y) d\tau + T_D \frac{d}{dt} (\gamma y_{sp} - y) \right)$$

= $K \left(e + \frac{1}{T_I} \int e d\tau + T_D \frac{de}{dt} \right)$
+ $\underbrace{K(\beta - 1)}_{K_1} y_{sp} + \underbrace{T_D K(\gamma - 1)}_{K_2} \frac{dy_{sp}}{dt}$

 $y_{sp} \underbrace{\left(K_1 y_{sp} + K_2 d y_{sp}/dt \right)}_{T_1} \underbrace{F_1 d y_{sp}}_{T_2} \underbrace{F_2 d y_{sp}/dt}_{T_2} \underbrace{F_1 d y_{sp}}_{T_2} \underbrace{F$

Interpretation: Error feedback + feedforward from y_{sp}

Reference Generation – Input–Output Approach

2-DOF control structure with reference model and feedforward:



- H_m model that describes the desired setpoint response
- H_{ff} feedforward generator that makes y follow y_m
 - · Goal: perfect following if there are no disturbances or model errors

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Reference Generation – Input–Output Approach

The pulse transfer function from u_c to y is

$$H = \frac{H_p(H_{\rm ff} + H_c H_m)}{1 + H_p H_c}$$

Choose

Then

$$H_{\rm ff} = \frac{H_m}{H_p}$$

$$H = \frac{H_p(\frac{H_m}{H_p} + H_c H_m)}{1 + H_p H_c} = H_m$$

$$H = \frac{H_p(\frac{H_p}{H_p} + H_c)}{1 + H_p H_c}$$

Perfect model following!

Restrictions on the Model

In order for $H_{\rm ff} = \frac{H_m}{H_p}$ to be implementable (causal and stable),

- H_m must have at least the same pole excess as H_p
- any zeros of H_p outside unit circle must also be included in H_m

In practice, also poorly damped zeros of H_p (e.g., outside the heart-shaped region below) should be included in H_m



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Process: $\mathcal{G}_{\rho}(s) = \frac{3}{(1+60s)^{2}}$ ZOH-sampled process (h = 3): $\mathcal{H}_{p}(z) = \frac{0.003627(z+0.9672)}{(z-0.9512)^{2}}$ PID controller tuned for good regulation performance: $\mathcal{G}_{c}(s) = \mathcal{K}\left(1 + \frac{1}{sT_{i}} + \frac{sT_{d}}{1+sT_{d}/N}\right)$ with $\mathcal{K} = 7, T_{i} = 45, T_{d} = 15, N = 10$, discretized using FOH 15	Example: PID Control of the Double Tank	Example: PID Control of the Double Tank
	Process: $\begin{aligned} G_p(s) &= \frac{3}{(1+60s)^2}\\ \text{ZOH-sampled process } (h = 3):\\ &\qquad \qquad $	Simulation with simple error feedback: $ \begin{array}{l} & & & \\ & & & \\ & & \\ & & \\ & & \\ & & & \\$

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Example: PID Control of the Double Tank

Reference model (critically damped - should not generate any overshoot): .

$$G_m(s) = \frac{1}{(1+10s)^2}$$

Sampled reference model:

$$H_m(z) = \frac{0.036936(z+0.8187)}{(z-0.7408)^2}$$

Feedforward filter:

$$H_{\rm ff}(z) = \frac{H_{\rm m}(z)}{H_{\rm p}(z)} = \frac{10.1828(z+0.8187)(z-0.9512)^2}{(z-0.7408)^2(z+0.9672)}$$

Example: PID Control of the Double Tank





Example: PID Control of the Double Tank

Modified reference model that includes the process zero:

$$H_m(z) = \frac{0.034147(z+0.9672)}{(z-0.7408)^2}$$

New feedforward filer:

$$H_{\rm ff}(z) = \frac{H_{\rm m}(z)}{H_{\rm p}(z)} = \frac{9.414(z-0.9512)^2}{(z-0.7408)^2}$$

Example: PID Control of the Double Tank





Remark

In the implementation, both $u_{\rm ff}$ and y_m can be generated by a single dynamical system:



Matlab:

>> Hp	=	%	define process
>> Hm	=	%	define reference model
>> re	fgen = [Hm/Hp; Hm]	%	concatenate systems
>> mi:	nreal(ss(refgen))	%	make minimal state-space realization

Simplistic Setpoint Handling in State Space

Replace u(k) = -Lx(k) with

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$$u(k) = L_c u_c(k) - L x(k)$$

The pulse transfer function from $u_c(k)$ to y(k) is

$$H_{yu_c}(z) = C(zI - \Phi + \Gamma L)^{-1}\Gamma L_c = L_c \frac{B(z)}{A_m(z)}$$

In order to have unit static gain ($H_{yu_c}(1) = 1$), L_c should be chosen as

$$L_c = \frac{1}{C(I - \Phi + \Gamma L)^{-1}\Gamma}$$

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Reference Generation – State Space Approach u_c Model and Generator x_m Σ L u_{fb} Σ Process y

The model should generate a reference trajectory x_m for the process state x (one reference signal per state variable)

Observer

The feedforward signal u_{ff} should make x follow x_m

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 Goal: perfect following if there are no disturbances or model errors

Reference Generation – State Space Approach

Linear reference model:

$$x_m(k+1) = \Phi_m x_m(k) + \Gamma_m u_c(k)$$

Control law:

$$u(k) = L\left(x_m(k) - \hat{x}(k)\right) + u_{ff}(k)$$

- How to generate model states *x_m* that are compatible with the real states *x*?
- How to generate the feedforward control uff?

Design of the Reference Model

Start by choosing the reference model identical to the process model, i.e.,

$$x_m(k+1) = \Phi x_m(k) + \Gamma u_{ff}(k)$$

Then modify the dynamics of the reference model as desired using state feedback ("within the model")

$$u_{\rm ff}(k) = L_c u_c(k) - L_m x_m(k)$$

Gives the reference model dynamics

$$x_m(k+1) = (\underbrace{\Phi - \Gamma L_m}_{\Phi}) x_m(k) + \underbrace{\Gamma L_c}_{\Gamma} u_c(k)$$

Design of the Reference Model



Design of the Reference Model	Complete State-Space Controller
 Design choices: L_m is chosen to give the model the desired eigenvalues (poles) L_c is chosen to give the desired static gain (usually 1) 	The complete controller, including state feedback, observer, and reference generator is given by
Remark: The reference model will have the same zeros as the process, so there is no risk of cancelling poorly damped or unstable zeros	$\begin{split} \hat{x}(k+1) &= \Phi \hat{x}(k) + \Gamma u(k) + K(y(k) - C \hat{x}(k)) \qquad \text{(Observer)} \\ x_m(k+1) &= \Phi x_m(k) + \Gamma u_{ff}(k) \qquad \text{(Reference model)} \\ u(k) &= L(x_m(k) - \hat{x}(k)) + u_{ff}(k) \qquad \text{(Control signal)} \\ u_{ff}(k) &= -L_m x_m(k) + L_c u_c(k) \qquad \text{(Feedforward)} \end{split}$

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Additional zeros and poles can be added by extending the model

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Design Example: Depth Control of Torpedo



State vector:

$$x = \begin{pmatrix} q \\ \theta \\ y \end{pmatrix} = \begin{pmatrix} \text{pitch angular velocity} \\ \text{pitch angle} \\ \text{depth} \end{pmatrix}$$

Input signal:

 $u = \delta =$ rudder angle

Torpedo: Continuous-Time Model

Simple model:

$$\frac{dq}{dt} = aq + b\delta$$
$$\frac{d\theta}{dt} = q$$
$$\frac{dy}{dt} = -V\theta (+ c\delta)$$

where a = -2, b = -1.3, and V = 5 (speed of torpedo)

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$$\dot{x} = \begin{pmatrix} a & 0 & 0 \\ 1 & 0 & 0 \\ 0 & -V & 0 \end{pmatrix} x + \begin{pmatrix} b \\ 0 \\ 0 \end{pmatrix} u$$
$$y = \begin{pmatrix} 0 & 0 & 1 \end{pmatrix} x$$

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Torpedo: Sampled Model

Sample with h = 0.2

$$x(k+1) = \begin{pmatrix} 0.67 & 0 & 0 \\ 0.165 & 1 & 0 \\ -0.088 & -1 & 1 \end{pmatrix} x(k) + \begin{pmatrix} -0.214 \\ -0.023 \\ 0.008 \end{pmatrix} u(k)$$

Matlab:

>> A = [a 0 0; 1 0 0; 0 -V 0]; >> B = [b; 0; 0]; >> C = [0 0 1]; >> Gp = ss(A,B,C,0); >> h = 0.2; >> Hp = c2d(Gp,h); >> [Phi,Gamma] = ssdata(Hp);

Torpedo: State Feedback Design

- u(k) = -Lx(k)
- rejection of (impulse) load disturbances

Desired continuous-time dynamic behaviour:

- two complex-conjugated poles with relative damping 0.5 and natural frequency ω_c
- one pole in $-\omega_c$
- a single parameter decides the dynamics

Desired characteristic polynomial

$$(s^2+2\cdot 0.5\cdot arphi_c s+arphi_c^2)(s+arphi_c)=s^3+2arphi_c s^2+2arphi_c^2 s+arphi_c^3)$$

Each pole translated into discrete time as $z_i = e^{s_i h}$

Torpedo: State Feedback Design in Matlab	Torpedo: Observer Design
<pre>Matlab: >> wc = 1; % speed of state feedback >> pc = wc*roots([1 2 2 1]); % control poles in cont time >> pcd = exp(pc*h); % control poles in disc time >> L = place(Phi, Gam, pcd) L = -0.145 -1.605 0.153</pre>	 x̂(k + 1) = Φx̂(k) + Γu(k) + K(y(k) - Cx̂(k)) state estimation + measurent noise rejection Observer Dynamics: the same pole layout as in the state feedback design parametrized by ω_o instead of ω_c typically faster dynamics than the state feedback, e.g., ω_o = 2ω_c Desired continuous-time characteristic polynomial: (s² + ω_os + ω_o²)(s + ω_o) = s³ + 2ω_os² + 2ω_o²s + ω_o³
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Torpedo: Observer Design in Matlab

>> wo = 2; % speed of observer >> po = wo*roots([1 2 2 1]); % observer poles in cont time >> pod = exp(po*h); % observer poles in disc time >> K = place(Phi',C',pod)' K = 0 -0.130 0.460





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Torpedo: Reference Model and Feedforward Design	Torpedo: Reference Model and Feedforward in Matlab	
Reference model:		
$x_m(k+1) = \Phi x_m(k) + \Gamma u_{ff}(k)$ Feedforward: $u_{ff} = -L_m x_m + L_{cm} u_c$ Desired characteristic polynomial: $(s + \omega_m)^3 = s^3 + 3\omega_m s^2 + 3\omega_m^2 s + \omega_m^3$	<pre>>> wm = 2; % speed of model >> pm = wm*roots([1 3 3 1]); % model poles in cont time >> pmd = exp(pm*h); % model poles in disc time >> Lm = place(Phi,Gam,pmd) Lm = -2.327 -6.744 0.886 >> Hm = ss(Phi-Gam*Lm,Gam,C,0,h);</pre>	
(critically damped – important!) • Parametrized using ω_m • Chosen as $\omega_m = 2\omega_c$	Lcm = 0.836	
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Torpedo: Final Controller

Model states and feedforward signal:







• Does not work very well – the feedforward term is needed to get the desired setpoint response

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Torpedo: Final Controller without Feedback

Simulation without the feedback signal, $u(k) = u_{ff}(k)$:



• Does not work – the feedback term is needed to stabilize the process and handle the load disturbance

Nonlinear Reference Generation

Recall the state-space approach to reference generation:



 u_{ff} and x_m do not have to come from linear filters but could be the result of solving an optimization problem, e.g.:

- Move a satellite to a given altitude with minimum fuel
- Position a mechanical servo in as short time as possible under a torque constraint
- · Move the ball on the beam as fast as possible without losing it

General Solution for Linear Processes

Assume linear process

$$\frac{dx}{dt} = Ax + Bu$$

- Derive the feedforward (open-loop) control signal u_{ff} that solves the stated optimization problem
 Course in Nonlinear Control (FRTN05, Lp 2)
- Generate the model state trajectories by solving

 $\frac{dx_m}{dt} = Ax_m + Bu_{\rm ff}$

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Similar approach can be used for sampled systems

Example: Time-Optimal Control of Ball on Beam Example: Time-Optimal Control of Ball on Beam Optimization problem: Assume steady state. Move the ball from start position $z(0) = z_0$ to final position $z(t_f) = z_f$ in minimum time while respecting the control signal constraints $-u_{\max} \le u(t) \le u_{\max}$ Optimal control theory gives the optimal open-loop control law State vector: $\left(-u_0, \quad 0 \leq t < T\right)$ ball position $u_{\rm ff}(t) = \begin{cases} u_0, & T \le t < 3T \\ -u_0, & 3T \le t < 4T \end{cases}$ ball velocity v X =beam angle , where Continuous-time state-space model: $u_0 = \operatorname{sgn}(z_f - z_0) u_{\max}$ $\frac{dz}{dt} = V$ $T = \sqrt[3]{\frac{|z_f - z_0|}{2k_{\phi}k_v u_{\max}}}$ $\frac{dv}{dt} = -k_v\phi \qquad (k_v\approx 10)$ $(k_{\phi} \approx 4.5)$ $\frac{d\phi}{dt} = k_{\phi} u$ $t_f = 4T$ 46

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Example: Time-Optimal Control of Ball on Beam





("bang-bang" control)

Example: Time-Optimal Control of Ball on Beam



Example: Time-Optimal Control of Ball on Beam



Example: Time-Optimal Control of Ball on Beam

Finally, solving



 $\frac{dz_m}{dt} = V_m$

Using the Time-Optimal Feedforward Generator in a Cascade Control Structure



• The PID controller should have derivative weighting $\gamma = 1$

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Lectures 9 and 10: Summary

- Regulator problem reduce impact of load disturbances and measurement noise
 - Feedforward from measurable disturbances
 - Input–output approach: design of feedback controller $H_{lb}(z)$, e.g. PID controller
 - State space approach: design of state feedback and observer, including disturbance estimator
- Servo problem make the output follow the setpoint in the desired way
 - Input–output approach: design of reference model $H_m(z)$ and feedforward filter $H_{ff}(z)$
 - State space approach: design of combined reference and feedforward generator
 - Linear or nonlinear reference generation