Physiological Models and Computations

Exercises

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2013

0. Introduction to MATLAB and SIMULINK

Solve the following exercises using MATLAB. These exercises are inspired by or fully extracted from *EDA017: Föreläsningsanteckningar, OCTAVE/MATLAB* by Christian Söderberg.

0.1

a. Plot $y(x) = e^{-x/2}\cos(2\pi x)$ when $-6 \leq x \leq 3$ by using the function handle to create an anonymous function. Give your plot a title as well as labels on the axes. Useful commands: `fplot`, `xlabel`, `ylabel`, `title`.

b. Modify your code such that you only show values $-4.5 \leq x \leq -1$ and $-10 \leq y \leq 10$. Useful command: `axis`.

c. Integrate the function for $-4.5 \leq x \leq -1$. Useful commands: `integral`, `quad`.

d. Find the solution to $f(x) = 0$ when $f(x) = x^3 + 2x - 1$. Comment on the answer. Useful command: `fsolve`.

0.2 Write a function which for every matrix A gives you the sum of the diagonal elements of that matrix. Useful commands: `diag`, `sum` and `size`.

0.3 Solve the differential equation

$$\begin{aligned} \ddot{y} + 7\dot{y} - 3y &= 0 \\ y(0) &= 0 \\ \dot{y}(0) &= 1 \end{aligned}$$

in the interval $0 \leq t \leq 5$ by using MATLABs solver `ode45`.

0.4 Try to fit a first order polynomial $ax + b$ to the following measurements

x	y
1	3.9286
2	5.4059
3	6.0771
4	7.7145

Solve the following exercises using SIMULINK in MATLAB. These exercises are taken from *Exercises in MATLAB/Simulink, Signals and Systems* by Thomas Munther.

0.5 Investigate the bacterial growth in a jam pot. Assume that the number of born bacteria is increasing proportional to the existing number of bacteria x and the number dying is proportional to the existing number in square. This gives the following differential equation

$$\frac{dx}{dt} = bx - px^2$$

where $b = 1$ [1/hour] is the birth rate constant and $p = 0.5$ [1/(bacteria·hour)] is the death rate constant. Assume $x(0) = 100$ [bacteria]. Use SIMULINK to show how the solution to the differential equation looks like.

0.6 Some physiological systems are better described in discrete time which gives rise to difference equations. Show the behavior of y in the two following difference equations

a.

$$y_t = -0.5 \cdot y_{t-1} + x_t$$

b.

$$y_t = 0.5 \cdot y_{t-1} + x_t$$

where x is the input signal to the system, in shape of a step starting in $t = 0$ with amplitude 1 and $y_{-1} = 1$. y_t is the value of y in time step t.

1. Biochemical Reactions

1.1 Use the law of mass balance to derive the differential equations govering the production of X and Y:

a.

$$X \underset{k_{-1}}{\overset{k_1}{\rightleftharpoons}} Y$$

b.

$$X + X \underset{k_{-1}}{\overset{k_1}{\rightleftharpoons}} Y$$

c.

$$3X + Y \underset{k_{-1}}{\overset{k_1}{\rightleftharpoons}} Z \tag{1.1}$$

1.2 Simulate and plot the concentrations for the substrate S, enzyme E, substrate-enzyme complex C and the end product P for the basic enzymatic reaction

$$S + E \underset{k_{-1}}{\overset{k_1}{\rightleftharpoons}} C \xrightarrow{k_2} P + E$$

using the following set of parameters; $k_1 = 0.1$, $k_{-1} = 0.01$ and $k_2 = 0.02$, and with the following initial conditions $[S]_0 = 0.15$ [mmol/l], $[E]_0 = 0.01$ [mmol/l], $[C]_0 = 0$ [mmol/l] and $[P]_0 = 0$ [mmol/l]. What happens if the initial concentration of the enzyme is doubled? What happens if the initial concentration of the substrate is doubled? How does these results correspond to the Michealis-Menten parameters?

1.3 The data in Table 1.1 describes the concentration and reaction rates of a chemical process. Is it an enzymatic reaction following the Michaelis-Menten relationship? Can you give some rough estimates of V_{max} and K_m from this graph? Plot the inverse of the concentration versus the inverse of the reaction rate. This plot is commonly reffered to as a Lineweaver-Burk plot. Can you give some rough estimates of V_{max} and K_m from this graph as well?

1.4 Competetive Inhibition: Some enzymes may bind other substances than the target substrate to the binding site, thereby inhibiting the formation of the intended substrate-enzyme complex and the subsequent end-product. Such a situation is characterized by the following reaction dynamics:

$$S + E \underset{k_{-1}}{\overset{k_1}{\rightleftharpoons}} C_1 \xrightarrow{k_2} P + E$$

$$I + E \underset{k_{-3}}{\overset{k_3}{\rightleftharpoons}} C_2$$

Table 1.1 Reaction Data for problem 3

Substrate Concentration [mM]	Reaction Velocity [mM/s]
0.1	0.04
0.2	0.08
0.5	0.17
1.0	0.24
2.0	0.32
3.5	0.39
5.0	0.42

Derive the following relationship for the reaction velocity of the product reaction, considering steady-state conditions for the enzyme and enzyme complexes and preservation of the total enzyme content:

$$V = \frac{V_{max}[S]}{[S] + K_m(1 + [I]/K_I)}$$

where $[I]$ is the concentration of the inhibitor, $K_m = (k_{-1} + k_2)/k_1$ and $K_I = k_{-3}/k_3$.

1.5 Alcohol metabolism: Clearance of the blood alcohol level (BAL) $[A]$ [mg/dl] from the liver is metabolized by more than 20 different enzymes. From experimental data the total clearance effect of these enzymes has been lumped into a common Michaelis-Menten relationship with population average $V_{max} = -15$[mg/(dl· h)] and a $K_m = 5$ [mg/dl].

$$\frac{d[A]}{dt} = \frac{V_{max}[A]}{K_m + [A]}$$

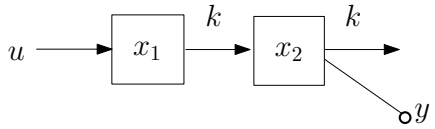
To calculate the BAL, the total distribution volume of the body for alhocol has to be known. The following relationship between the total water volume, representing this distribution volume V_D $[l]$, and the weight m_{BW} [kg], gender and age Y [years] of the person has been suggested.

$$V_D = 20 + 0.36m_{BW} - 0.1Y, \quad Men$$
$$V_D = 14 + 0.25m_{BW}, \quad Women$$

Assuming that a 25 year old man of 80 kg consumes a drink containing 2 cl of alcohol (density 800 kg/m^3) at a fasting state. Digestion of alcohol is very rapid on an empty stomach, and you may assume that the total alcohol content has reached the blood stream after 20 minutes whereafter metabolization is considered to start. Simulate and plot the BAL level for the four hours following the drink.

2. Model Building and Linearization

2.1 Given the compartment model below



assume that x_1 and x_2 represent quantities of a substance subject to conservation. y is a measurement of x_2.

a. Give the balance equations when $k = 1$. What are the states, the input and the output of the system?

b. From the balance equations derive the state space representation for the system.

c. Determine the transfer function of the system analytically and by using functions from the control toolbox in MATLAB.

2.2 Give the state-space representation of the system

$$\dddot{y} + 3\ddot{y} + 2\dot{y} + y = u$$

where $u(t)$ and $y(t)$ are the input and output, respectively. Choose states $x_1 = y$, $x_2 = \dot{y}$ and $x_3 = \ddot{y}$.

2.3 A process with output $y(t)$ and input $u(t)$ is described by the differential equation

$$\ddot{y} + \sqrt{y} + y\dot{y} = u^2$$

a. Introduce states $x_1 = y$, $x_2 = \dot{y}$ and give the state space representation of the system.

b. Find all stationary points (x_1^0, x_2^0, u^0) of the system.

c. Linearize the system around the stationary point corresponding to $u^0 = 1$.

2.4 Linearize the system

$$\begin{aligned} \dot{x}_1 &= x_1^2 x_2 + \sqrt{2}\sin u && (= f_1(x_1, x_2, u)) \\ \dot{x}_2 &= x_1 x_2^2 + \sqrt{2}\cos u && (= f_2(x_1, x_2, u)) \\ y &= \arctan\frac{x_2}{x_1} + 2u^2 && (= g(x_1, x_2, u)) \end{aligned}$$

around the stationary point $u^0 = \pi/4$.

2.5 Blood Doping: Everyday about $2.5 \cdot 10^{11}$ (0.25 trillion) new red blood cells (RBCs) are released from the bone marrow into the peripheral circulation, and in steady-state the same number of depleted RCB:s

are cleared by the spleen. Assume that the average lifespan of a RCB is 120 days, and the cleared amount between two days k and $k-1$ is a constant fraction f of the total cell population $R(k-1)$ at day $k-1$. The cell population $R(k)$ is R_{ref} [trillion cells] at steady state. Furthermore, the rate of production $r(k)$ [trillion cells/day] is controlled by the level of erythropoietin EPO $u(k)$ [Units/ml] according to the outlined dynamics below (changes in the EPO level do not fully effect the production rate directly, but the production rate $r(k)$ is partly dependent on the production rate the previous day $r(k-1)$):

$$r(k) = 0.9 \cdot r(k-1) + u(k), \quad r(0) = f \cdot R_{ref}, u(0) = 0.025 \tag{2.1}$$

Set up the difference equations for the red blood cell population $R(k)$ and the production rate $r(k)$. Assume that we are at steady state with a total cell population R_{ref} of $120 \cdot 0.25$ trillion cells. Create a Simulink model according to Fig. 2.1 and simulate the system for 100 days. Assume that the level of EPO normally is constant at 0.025 Units/ml, but that it is artificially elevated to the double normal level by injections for 20 consecutive days between day 21 and 40.

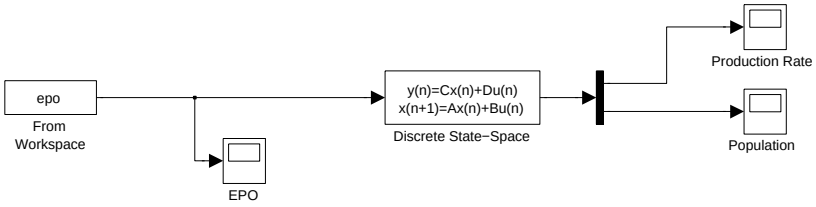


Figure 2.1 Simulink model for the red blood cell system

2.6 Infection; Bacteria-Leukocytes Predator-Prey System: Neuthrophiles are specialised white blood cells (leukocytes), specialising in defending against bacterial infections. Let $B(t)$ denote the number of bacteria in a wound and $N(t)$ the number of neuthrophiles. The bacterial growth factor is α [bacteria/hour] and the killing factor of the neuthrophiles β [bacteria/hour] and assume that the entry rate of new neuthrophiles is $u(t)$ [neutrophiles/hour].

$$\frac{dB}{dt} = \alpha B(t) - \beta \cdot B(t) \cdot N(t) \tag{2.2}$$

$$\frac{dN}{dt} = -\gamma N(t) + u(t) \tag{2.3}$$

Simulate the system in Simulink with $\alpha = 3, \beta = 1.1, \gamma = 1.5$, and with initial conditions $B(0) = 100, N(0) = 0$ and let $u(t)$ be a step with magnitude 10. What happens if α becomes large (> 8)?

3. Control in Physiology 1

3.1 Determine the transfer functions and give differential equations, describing the relation between input and output for the following systems, respectively.

a.

$$\dot{x} = \begin{pmatrix} -2 & 0 \\ 0 & -3 \end{pmatrix} x + \begin{pmatrix} 5 \\ 2 \end{pmatrix} u$$
$$y = \begin{pmatrix} -1 & 1 \end{pmatrix} x + 2u$$

b.

$$\dot{x} = \begin{pmatrix} -7 & 2 \\ -15 & 4 \end{pmatrix} x + \begin{pmatrix} 3 \\ 8 \end{pmatrix} u$$
$$y = \begin{pmatrix} -2 & 1 \end{pmatrix} x$$

3.2 Determine the impulse and step responses of the systems in assignment 3.1 both analytically and through MATLAB. The step response is defined as the output of the system when the input is the step function $u(t) = 1$ for $t > 0$ and $u(t) = 0$ for $t < 0$.

3.3 Derive the formula $G(s) = C(sI - A)^{-1}B + D$ for a general system

$$\dot{x} = Ax + Bu$$
$$y = Cx + Du$$

3.4 Consider the system

$$G(s) = \frac{1}{s^2 + 4s + 3}$$

a. Calculate the poles and zeros of the system. Is the system stable?

b. Calculate the impulse response by hand and plot it in MATLAB.

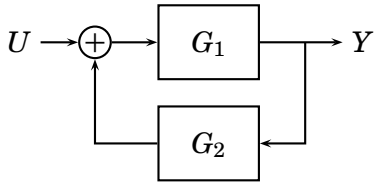
3.5 Consider the linear time invariant system

$$\frac{dx}{dt} = \begin{pmatrix} 0 & -1 \\ 1 & 0 \end{pmatrix} x + \begin{pmatrix} 1 \\ 0 \end{pmatrix} u$$
$$y = \begin{pmatrix} 1 & -1 \end{pmatrix} x$$

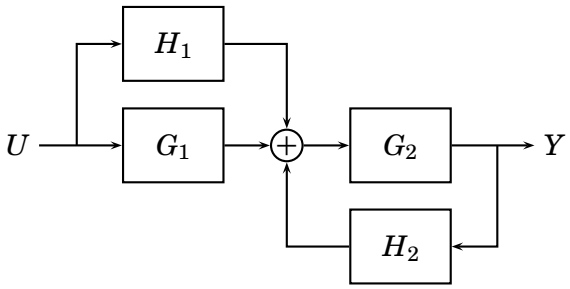
Is the system stable?

3.6 Determine the transfer function from U to Y for the systems below.

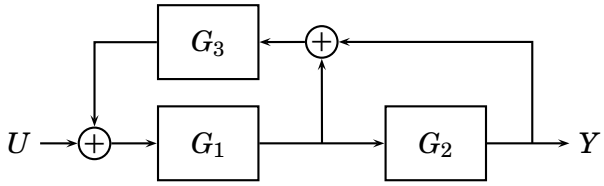
a.



b.



c.



3.7 Assume that the system

$$G(s) = \frac{0.01(1+10s)}{(1+s)(1+0.1s)}$$

is subject to the input $u(t) = \sin 3t, \quad -\infty < t < \infty$

a. Determine the output $y(t)$.

b. The Bode plot of the system is shown in figure 3.1. Determine the output $y(t)$ by using the Bode plot instead.

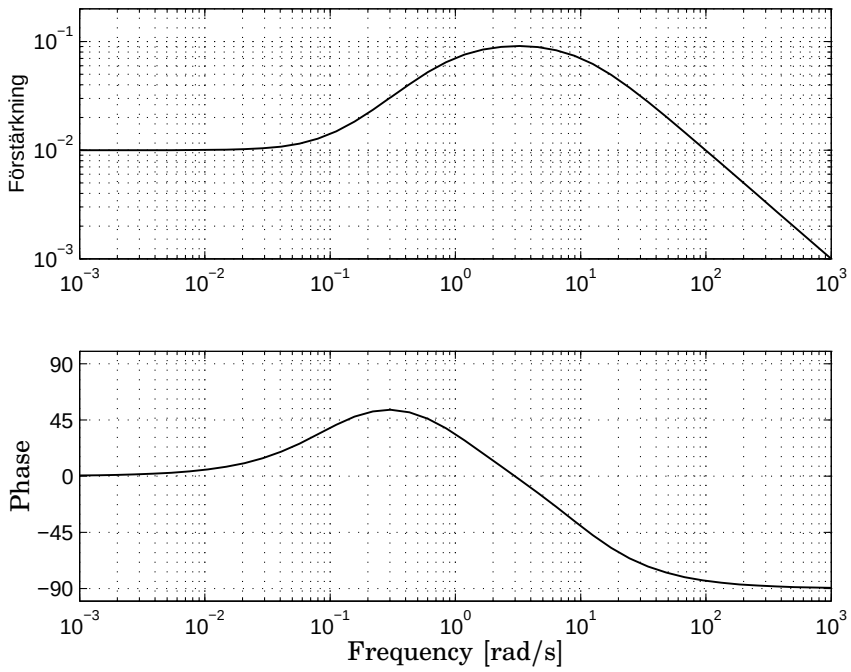


Figure 3.1 The Bode plot in assignment 3.7.

4. Control in Physiology 2

4.1 Assume that the amount of some substrate y inside a cell is described by the differential equation

$$\dot{y}(t) + 0.01y(t) = 0.01u(t)$$

where u is the inflow of the substrate to the cell.

a. Let u be the input and y the output and determine the transfer function $G_P(s)$ of the process.

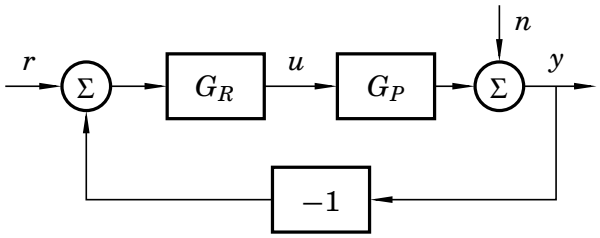
b. This is to be controlled by negative feedback with a controller $G_R(s)$. Draw the block diagram and write down the transfer function of the closed loop system. Be sure to define the input u, output y, error e and reference signal r in the block diagram of the closed loop system.

c. If $G_R(s)$ is a P controller what will the transfer function look like then?

d. Choose K, given that $G_R(s) = K$, such that the closed loop system obtains the characteristic polynomial

$$s + 0.1$$

4.2 A process is controlled by a P controller according to the figure below.



a. Measurements of the process output indicate a disturbance n. Calculate the transfer functions from n to y (the sensitivity function).

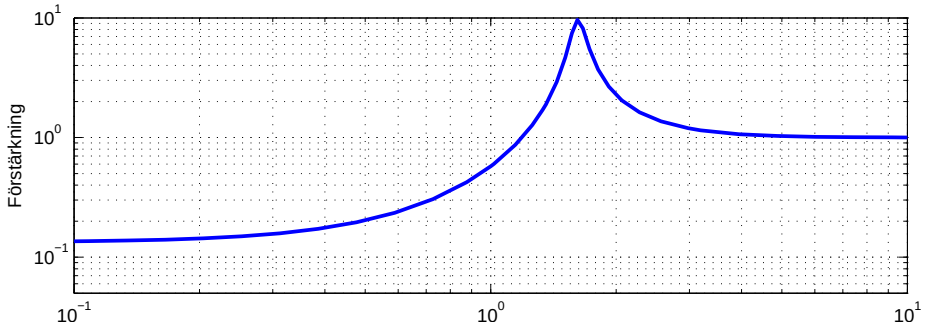
b. Let $G_P(s) = 1/(s+1)$ and $G_R(s) = K$ and assume that the disturbance consists of a sinusoid $n(t) = A\sin\omega t$. What will y become when this disturbance is present?

c. Assume that $K = 1$ and $A = 1$ in the previous sub-assignment. Calculate the amplitude of oscillation y for the cases $\omega = 0.1$ and 10 rad/s, respectively.

4.3 The process given by $G_P(s) = 1/(s+1)^3$ is controlled through negetive feedback by the controller given by $G_R(s) = 6.5$.

a. Determine the sensitivity function $S(s)$.

b. The gain plot of the sensitivity function is given below. How much are constant load disturbances damped by the control circuit (in closed loop, as compared to open loop)? At which angular frequency does the control circuit exhibit the largest sensitivity towards disturbances and by how much are disturbances amplified at most?



4.4 Determine a control law $u = l_r r - Lx$ for the system

$$\frac{dx}{dt} = \begin{pmatrix} -1 & 0 \\ 0 & -2 \end{pmatrix} x + \begin{pmatrix} 1 \\ 2 \end{pmatrix} u$$
$$y = \begin{pmatrix} 1 & 1 \end{pmatrix} x$$

such that the poles of the closed loop system are placed in -4 and the stationary gain is 1. How would you sketch the block diagram of the closed loop system?

5. Pharmacokinetics and Tracers

5.1 The half-life of a penicillin solution that contains 300 units/ml is 8 days, in plasma. What will the concentration in plasma be in 7 days? Assume the drug is eliminated from plasma through a linear process. Plot the concentration over time.

5.2 The half-life of another penicillin solution is 6 days. Assume it is eliminated from plasma as a linear process. How long will it take for the concentration to drop to 40 % of the initial concentration?

5.3 Assume a drug is metabolised from plasma through a linear process. It has an initial potency of 90 mg/ml. After 25 days in a cold room, the concentration is found to be 80 mg/ml. What is the half-life of the drug during the storage conditions?

5.4 Draw a compartment model of the route of a drug including the absoption in the gut, the distribution in the body and the elimination of the drug.

Solutions to Chapter 0. Introduction to MATLAB and SIMULINK

Solve the following exercises using MATLAB. These exercises are inspired by or fully extracted from *EDA017: Föreläsningsanteckningar, OCTAVE/MATLAB* by Christian Söderberg.

0.1 a. Create an anonymous function using the function handle. This function is only saved in your workspace until you close MATLAB (or clear you workspace by the `clear all` command). In case you would like to save your function as a file in your current folder (from where you can reach it at another time), use a function m-file (go to new → function).

```
y = @(x) exp(-x/2)*cos(2*pi*x);

figure
fplot(y,[-6 3])
title('My fancy plot')
xlabel('x')
ylabel('y')
```

`figure` is a command which is useful when you want to create several plots in the same script. Use the `help`-command whenever you need information about one of MATLABs buildt-in functions. In this case you would write `help figure` in the command window and the description of the function should appear.

b.

```
axis([-4.5 -1 -10 10])
```

c.

```
% Rewrite y to be accepted by quad/integral (read in the
% description of quad/integral to understand why).
y = @(x) exp(-x/2).*cos(2*pi*x);

integral(y,-4.5,-1)
% or
quad(y,-4.5,-1)
```

d.

```
f = @(x) x^3+2*x-1;
solution = fsolve(f,0)
```

The answer is 0.4534. Write `format long` in the command window (then use the `fsolve` command) to get more decimals in the answer. Due to it being numerically calculated $f(0.4534)$ is approximately zero.

0.2 Go to new → function. A file with a function-shell will appear. The function shell looks like:

```
function [ output_args ] = untitled( input_args )
%UNTITLED Summary of this function goes here
%   Detailed explanation goes here


end
```

Replace `untitled` with the name of your function, `input_args` with the input your function needs and `output_args` with the output your function will give. Between the `function`-row and the `end` you should write the code for the function.

For the particular function of this exercise, it will look as follows

```
function sumOfDiag = sumOfDiagonal(A)
[n,m] = size(A);

if n ≠ m
    error('A is not a square matrix')
end

sumOfDiag = sum(diag(A));
end
```

Where $\neq$ is written as ~= in MATLAB. Save your function as an m-file in your current folder, by the name of your function. In this case it would be "sumOfDiagonal.m". Now you can use your function directly from the command window or from a script which is saved in the same folder as your function.

To create a matrix in MATLAB use the following principle

```
my_matrix = [1 2; 3 4];
```

`[` and `]` begins and ends the matrix. Elements are separated by space (or comma) and rows are separated by `;`. The resulting matrix is

$$\begin{pmatrix} 1 & 2 \\ 3 & 4 \end{pmatrix}$$

0.3 Introduce $y_1(t) = y(t)$ and $y_2(t) = \dot{y}(t)$ in order to rewrite the initial second-order differential equation into two first-order differential equations as follows

$$\dot{y}_1 = y_2 \tag{0.1}$$
$$\dot{y}_2 = 3y_1(t) - 7y_2 \tag{0.2}$$

The initial conditions for $y_1(t)$ and $y_2(t)$ are

$$y_1(0) = y(0) = 0$$
$$y_2(0) = \dot{y}(0) = 1$$

(0.1) and (0.2) can be written together on matrix form as follows

$$\begin{pmatrix} \dot{y}_1 \\ \dot{y}_2 \end{pmatrix} = \begin{pmatrix} y_2 \\ 3y_1 - 7y_2 \end{pmatrix} = \begin{pmatrix} 0 & 1 \\ 3 & -7 \end{pmatrix} \begin{pmatrix} y_1 \\ y_2 \end{pmatrix}$$

Define $\mathbf{v} = \begin{pmatrix} y_1 \\ y_2 \end{pmatrix}$. Then, define f as the following function

$$f(t, \mathbf{v}) = f(t, \begin{pmatrix} y_1 \\ y_2 \end{pmatrix}) = \begin{pmatrix} \dot{y}_1 \\ \dot{y}_2 \end{pmatrix} = \begin{pmatrix} y_2 \\ 3y_1 - 7y_2 \end{pmatrix} = \begin{pmatrix} 0 & 1 \\ 3 & -7 \end{pmatrix} \begin{pmatrix} y_1 \\ y_2 \end{pmatrix}$$

In MATLAB this can be written as

```
f = @(t,v) [v(2); 3*v(1)-7*v(2)];
```

Or by matrix multiplication

```
f = @(t,v) [0 1; 3 -7]*v;
```

To solve the differential equation write the following code

```
[t_ode V] = ode45(f,[0 5],[0 1]);
```

The first input to `ode45` is the right part of the differential equation, the second input is the time span of the solution while the third is the initial condition of the differential equation. `V` is a matrix with two columns, the first column corresponds to $y_1(t) = y(t)$ and the second column corresponds to $y_2(t) = \dot{y}(t)$. `t_ode` is the times between 0 and 5 at which `ode45` has calculated y_1 and y_2. Use the following code to plot $y(t)$ over $0 \leq t \leq 5$

```
plot(t_ode,V(:,1))
```

0.4 The first order polynomial means that

$$b + a = 3.9286$$
$$b + 2a = 5.4059$$
$$b + 3a = 6.0771$$
$$b + 4a = 7.7145$$

In matrix form this becomes

$$\begin{pmatrix} 1 & 1 \\ 2 & 1 \\ 3 & 1 \\ 4 & 1 \end{pmatrix} \cdot \begin{pmatrix} a \\ b \end{pmatrix} = \begin{pmatrix} 3.9286 \\ 5.4059 \\ 6.0771 \\ 7.7145 \end{pmatrix} \tag{0.3}$$

We have two unknowns and four equations. Therefore, we need to approximate a and b such that the distance between the line $ax + b$ and the points is minimized in some sence.

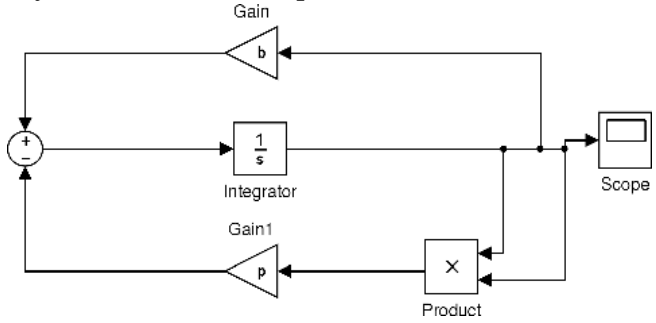
If (0.3) is seen as $S \cdot \begin{pmatrix} a \\ b \end{pmatrix} = T$, the following code will return the values of a and b

```
x = S\T;
```

Where `a = x(1)` and `b = x(2)`. This uses the least squares method to fit $ax + b$ to the points. Plot the points and the line in the same plot to see the fit.

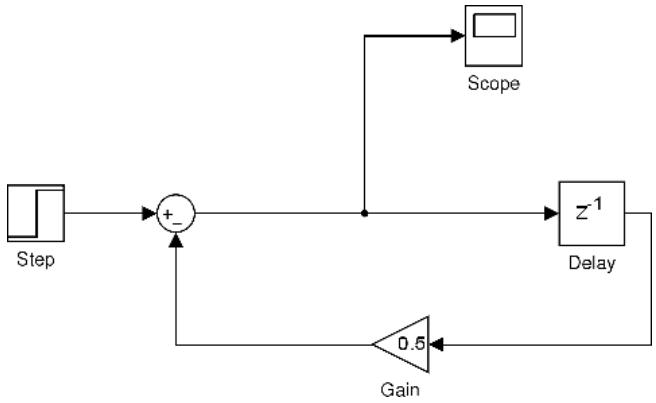
Solve the following exercises using SIMULINK in MATLAB. These exercises are taken from *Exercises in MATLAB/Simulink, Signals and Systems* by Thomas Munther.

0.5 Start SIMULINK by writing `simulink` in the MATLAB command window. This makes the SIMULINK Library Browser window pop up. Go to File → New → Model. In this window you can start to create your SIMULINK model. Use the Library Browser to find appropriate blocks and drag them into the model sheet. You can connect two blocks by their connection spots.

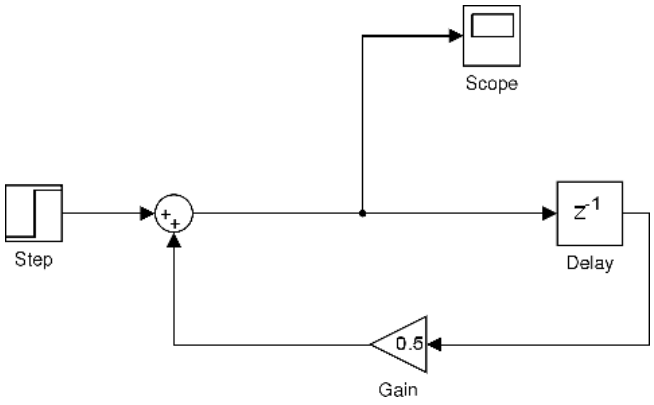


`p` and `b` can be defined in the current workspace. Go to display → blocks and check "Sorted Execution Order". This will numerate the blocks in the order in which they are first activated.

0.6 a. Before running the simulation go to Simulation → Configuration Parameters. In Solver Options choose Fixed-step and Solver → Discrete. Set the sample time in each block to 1 [sec].



b. The only difference from the previous model is that the minus sign in the sum-block is changed to a plus sign.


Scope
Step
+
+
z^{-1}
Delay
0.5
Gain

Solutions to Chapter 1. Biochemical Reactions

1.1 a. Denote the concentrations $x = [X]$ and $y = [Y]$

$$\frac{dx}{dt} = -k_1 x + k_{-1} y$$
$$\frac{dy}{dt} = k_1 x - k_{-1} y$$

b. Denote the concentrations $x = [X]$ and $y = [Y]$

$$\frac{dx}{dt} = -2k_1 x^2 + 2k_{-1} y$$
$$\frac{dy}{dt} = k_1 x^2 - k_{-1} y$$

c.

Denote the concentrations $x = [X]$, $y = [Y]$ and $z = [Z]$

$$\frac{dx}{dt} = -3k_1 x^3 y + 3k_{-1} z \tag{1.1}$$
$$\frac{dy}{dt} = -k_1 x^3 y + k_{-1} z \tag{1.2}$$
$$\frac{dz}{dt} = k_1 x^3 y - k_{-1} z \tag{1.3}$$
$$\tag{1.4}$$

1.2 A matlab script may look as follows:

```
% Simulation of the substrate, enzyme and product concentrations in a MM
% example
% ds/dt = -k_1 *(se) + k_{-1}*c
% de/dt = -k_1 *(se) + (k_{-1} + k_2)*c
% dc/dt = k_1 *(se) - (k_{-1} + k_2)*c
% dp/dt = k_2 c
%--------------------
% Initial conditions
s(1) = 0.15; % mmol/L
e(1) = 1e-2; % mmol/L
c(1) = 0; % mmol/L
p(1) = 0; % mmol/L
%--------------------
% Parameters
k1 = 0.1;
k3 = 0.01; % k_{-1}
k2= 0.02;
%--------------------

% Run discretized simulation
```

```
for k = 2:10000
    s(k) = s(k-1) + k3*c(k-1) - k1*s(k-1)*e(k-1);
    e(k) = e(k-1) + (k3+k2)*c(k-1) - k1*s(k-1)*e(k-1);
    c(k) = c(k-1) - (k3+k2)*c(k-1)  + k1*s(k-1)*e(k-1);
    p(k) = p(k-1) + k2*c(k-1);
end

figure(1)
[ax,h1,h2] = plotyy(1:10000,[s' p'],1:10000,[e' c'])
legend('Substrate','Product','Enzyme','Complex')
xlabel('time [s]')
ylabel(ax(1),'Substrate/Product Concentration [mmol/L]')
ylabel(ax(2),'Enzyme/Complex Concentration [mmol/L]')
title('Simulation of enzymatic reaction')

% Run ode-solver simulation
% y = [S E C P]

dAll = @(t,y) [-k1*y(1)*y(2)+k3*y(3); ...
    -k1*y(1)*y(2)+(k3+k2)*y(3); ...
    k1*y(1)*y(2)-(k3+k2)*y(3); ...
    k2*y(3)];

[t Y] = ode45(dAll,[0 10000],[0.15 1e-2 0 0])

figure(2)
[ax,h1,h2] = plotyy(t,[Y(:,1) Y(:,4)],t,[Y(:,2) Y(:,3)])
legend('Substrate','Product','Enzyme','Complex')
xlabel('time [s]')
ylabel(ax(1),'Substrate/Product Concentration [mmol/L]')
ylabel(ax(2),'Enzyme/Complex Concentration [mmol/L]')
title('Simulation of enzymatic reaction')
```

Doubling the enzymatic concentration doubles the production rate since $V_{max} = k_2 \cdot e_0$. Likewise since $K_m = (k_2 + k_{-1})/k_1 = 0.3$ and $V = V_{max}s/(K_m + s)$, a doubling of s_0 from $K_m/2$ to K_m means that the initial reaction rate will become 1.5 times greater.

1.3 The plot indicates that the relationship between the reaction rate and the substrate concentration goes to saturation in a M-M-like behavoir, see Fig. 1.1. V_{max} and K_m are estimated as shown in the plot.
Lineweaver-Burke plot: The Michaelis-Menten relationship between substrate concentrations $[S]$ states that:

$$v = \frac{V_{max}[S]}{K_m + [S]}$$

Taking the inverse yields:

$$\frac{1}{v} = \frac{K_m}{V_{max}}\frac{1}{[S]} + \frac{1}{V_{max}}$$

Now, the parameters K_m/V_{max} and $1/V_{max}$ for this linear relationship may be estimated from the plot as seen in Fig. 1.2.

1.4 Draw a graph of the compartment representation, see Fig 1.3. Next,

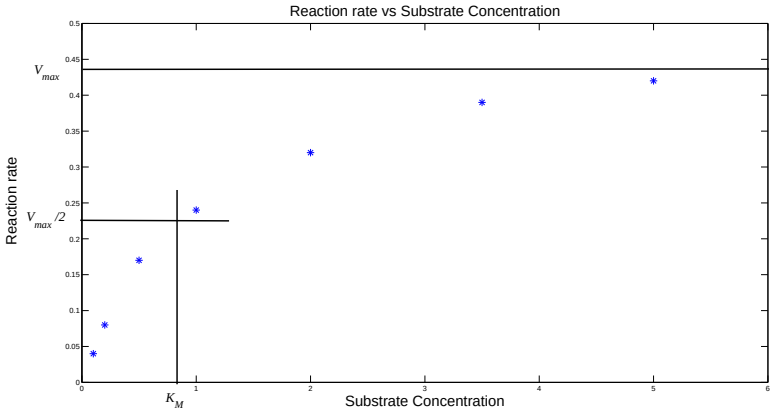


Figure 1.1 Graphical estimation of V_{max} and K_M

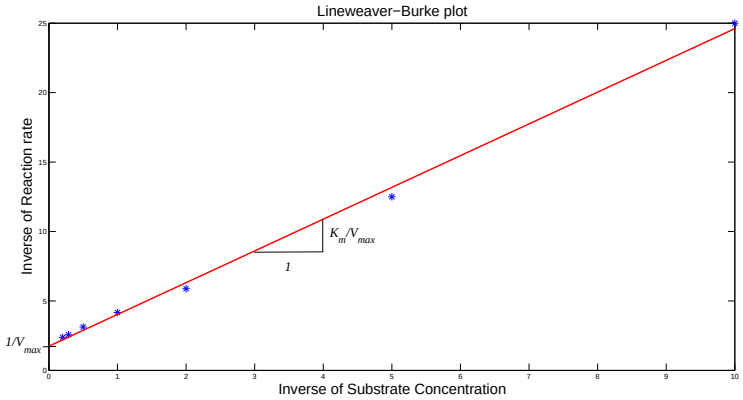


Figure 1.2 Graphical estimation of V_{max} and K_M using the Lineweaver-Burke plot.

determine the differential equations governing the reaction dynamics:

$$\frac{d[S]}{dt} = -k_1[S][E] + k_{-1}[C_1] \tag{1.5}$$

$$\frac{d[I]}{dt} = k_{-3}[C_2] - k_3[E][I] \tag{1.6}$$

$$\frac{d[C_1]}{dt} = k_1[S][E] - (k_{-1} + k_2)[C_1] \tag{1.7}$$

$$\frac{d[C_2]}{dt} = k_3[E][I] - k_{-3}[C_2] \tag{1.8}$$

$$\frac{d[E]}{dt} = (k_2 + k_{-1})[C_1] + k_{-3}[C_2] - k_1[S][E] - k_3[E][I] \tag{1.9}$$

$$\frac{d[P]}{dt} = k_2[C_1] \tag{1.10}$$

Next, use the steady-state assumptions; $d[C_1]/dt = d[C_2]/dt = 0$ to

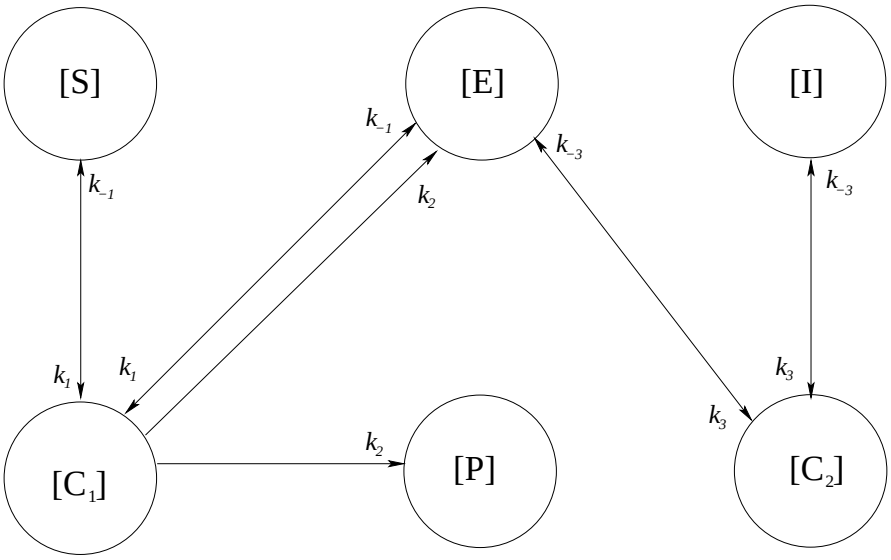


Figure 1.3 Compartment model representation of the enzyme inhibition dynamics.

get

$$[C_1] = \frac{k_1}{k_{-1} + k_2}[S][E] \tag{1.11}$$

$$[C_2] = \frac{k_3}{k_{-3}}[E][I] \tag{1.12}$$

The conservation of enzymatic mass gives

$$[E_0] = [E] + [C_1] + [C_2] = [E](1 + \frac{k_1}{k_{-1} + k_2}[S] + \frac{k_3}{k_{-3}}[I]) \tag{1.13}$$

Put Eq. (1.10), Eq. (1.11) and Eq. (1.13) together:

$$V = \frac{d[P]}{dt} = \frac{k_2[E_0][S]}{[S] + \frac{k_1}{k_{-1}+k_2}(1 + \frac{k_3}{k_{-3}}[I])} \tag{1.14}$$

1.5 Blood alcohol level

A matlab script may look as follows:

```
% BAL simulation
V = -15;% mg/(l*h)
K_m = 5;% mg/dl
%-----
VD = 10*(20 + 0.36*80-0.1*25); %dl
BAL(1:20) = zeros(20,1);
BAL(20) = 0.02*1000*0.8*1000/VD; % mg/dl
der = 0;
for k=21:1:240
    BAL(k) = BAL(k-1) + der;
    der = V/60*BAL(k)/(K_m + BAL(k));
end
plot([1:length(BAL)]/60,BAL)
title('Blood Alcohol Level after ingesting 2 cl alcohol ...
```

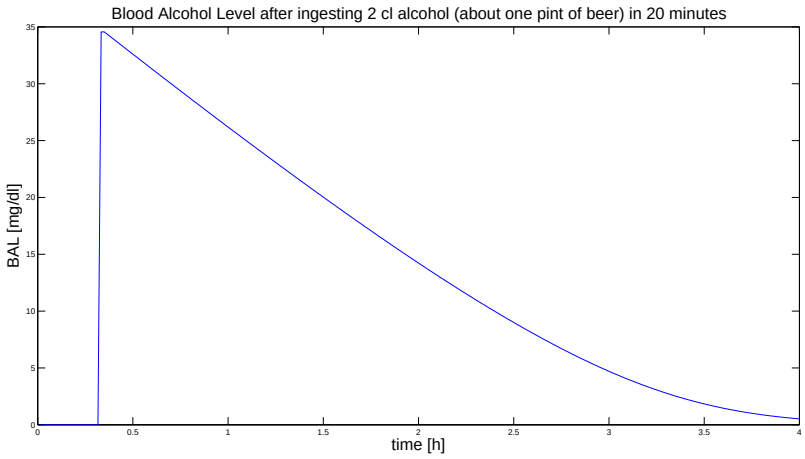


Figure 1.4 Blood alcohol content according to the simulation example.

```
(about one pint of beer) in 20 minutes','Fontsize',10)
ylabel('BAL [mg/dl]','Fontsize',10)
xlabel('time [h]','Fontsize',10)
```

Running the code generates the plot in Fig. 1.4.

Another possibility is to use MATLABs built in solvers for odrinary differential equations, such as ode45. The MATLAB-script would then look something like

```
% BAL simulation
V = -15;% mg/(l*h)
K_m = 5;% mg/dl
VD = 10*(20 + 0.36*80-0.1*25); % dl

% The 'initial value' of the concentration [A] is actually
% the concentration in t = 20 min when the metabolization
% of the alcohol starts.

initial_value_A = 0.02*1000*0.8*1000/VD; % mg/dl

% Define the differential equation y(t) = [A](t)
dAdt = @(t,y) V/60*y/(K_m+y);

% Solve the differential equation
[t, Y] = ode45(dAdt, [0 220], initial_value_A);

t = (t+20)/60; % Shifting the time vector 20 min, and changing into
% hours instead of minutes.
Y = [zeros(size(0:0.1:(t(1)-0.01))) Y']; % Adding zeros to the
% value-vector for time 0-20 min.
t = [0:0.1:(t(1)-0.01) t']; % Adding the time between 0-20 minutes
% to the time vector.

plot(t,Y)
title('Blood Alcohol Level after ingesting 2 cl alcohol ...
(about one pint of beer) in 20 minutes','Fontsize',10)
ylabel('BAL [mg/dl]','Fontsize',10)
xlabel('time [h]','Fontsize',10)
```

Solutions to Chapter 2. Model Building and Linearization

2.1

a. By concentration of substrate, we have

$$\begin{aligned}\frac{dx_1}{dt} &= -x_1 + u \\ \frac{dx_2}{dt} &= x_1 - x_2 \\ y &= x_2\end{aligned}$$

The states are x_1 and x_2. The input is u and the output is y.

b.

$$\begin{aligned}\begin{pmatrix}\dot{x}_1 \\ \dot{x}_2\end{pmatrix} &= \begin{pmatrix}-1 & 0 \\ 1 & -1\end{pmatrix}\begin{pmatrix}x_1 \\ x_2\end{pmatrix} + \begin{pmatrix}1 \\ 0\end{pmatrix} u \\ y &= \begin{pmatrix}0 & 1\end{pmatrix}\begin{pmatrix}x_1 \\ x_2\end{pmatrix}\end{aligned}$$

c.

$$\begin{aligned}G(s) &= C(sI - A)^{-1}B + D \\ &= \begin{pmatrix}0 & 1\end{pmatrix}\begin{pmatrix}s+1 & 0 \\ -1 & s+1\end{pmatrix}^{-1}\begin{pmatrix}1 \\ 0\end{pmatrix} \\ &= \frac{1}{(s+1)^2}.\end{aligned}$$

```
% State the state space matrices
A = [-1 0 ; 1 -1];
B = [1 ; 0];
C = [0 1];
D = []; % Empty matrix

% Construct the state space system
system = ss(A,B,C,D);

% Contruct the transfer function
G = tf(system)

% OR after having decided the transfer function
% analytically use
s = tf('s'); % To create the Laplace variable
G = 1/(s+1)^2;
```

2.2

$$\begin{pmatrix} \dot{x}_1 \\ \dot{x}_2 \\ \dot{x}_3 \end{pmatrix} = \begin{pmatrix} 0 & 1 & 0 \\ 0 & 0 & 1 \\ -1 & -2 & -3 \end{pmatrix} \begin{pmatrix} x_1 \\ x_2 \\ x_3 \end{pmatrix} + \begin{pmatrix} 0 \\ 0 \\ 1 \end{pmatrix} u$$
$$y = \begin{pmatrix} 1 & 0 & 0 \end{pmatrix} \begin{pmatrix} x_1 \\ x_2 \\ x_3 \end{pmatrix}$$

2.3 a.

$$\begin{aligned} \dot{x}_1 &= x_2 \\ \dot{x}_2 &= -\sqrt{x_1} - x_1 x_2 + u^2 \\ y &= x_1 \end{aligned}$$

b. A stationary point implies $\dot{x}_1 = \dot{x}_2 = 0$. From the first equation we directly obtain $x_2 = 0$. Subsequently, the second equation yields $\sqrt{x_1} = u^2$. Hence there are infinitely many stationary points and they can be parametrized through t as $(x_1^0, x_2^0, u^0) = (t^4, 0, t)$.

c. $u^0 = 1$ gives the stationary point $(x_1^0, x_2^0, u^0) = (1, 0, 1)$. We let

$$\begin{aligned} f_1(x_1, x_2, u) &= x_2 \\ f_2(x_1, x_2, u) &= -\sqrt{x_1} - x_1 x_2 + u^2 \\ g(x_1, x_2, u) &= x_1 \end{aligned}$$

Do taylorexpansion of these functions in the stationary point and use only the linear terms to linearize the system. Start by computing the partial derivatives

$$\begin{aligned} &\frac{\partial f_1}{\partial x_1} = 0 && \frac{\partial f_1}{\partial x_2} = 1 && \frac{\partial f_1}{\partial u} = 0 \\ &\frac{\partial f_2}{\partial x_1} = -\frac{1}{2\sqrt{x_1}} - x_2 && \frac{\partial f_2}{\partial x_2} = -x_1 && \frac{\partial f_2}{\partial u} = 2u \\ &\frac{\partial g}{\partial x_1} = 1 && \frac{\partial g}{\partial x_2} = 0 && \frac{\partial g}{\partial u} = 0 \end{aligned}$$

At the stationary point we have

$$\begin{aligned} &\frac{\partial f_1}{\partial x_1}(x_1^0, x_2^0, u^0) = 0 && \frac{\partial f_1}{\partial x_2}(x_1^0, x_2^0, u^0) = 1 && \frac{\partial f_1}{\partial u}(x_1^0, x_2^0, u^0) = 0 \\ &\frac{\partial f_2}{\partial x_1}(x_1^0, x_2^0, u^0) = -\frac{1}{2} && \frac{\partial f_2}{\partial x_2}(x_1^0, x_2^0, u^0) = -1 && \frac{\partial f_2}{\partial u}(x_1^0, x_2^0, u^0) = 2 \\ &\frac{\partial g}{\partial x_1}(x_1^0, x_2^0, u^0) = 1 && \frac{\partial g}{\partial x_2}(x_1^0, x_2^0, u^0) = 0 && \frac{\partial g}{\partial u}(x_1^0, x_2^0, u^0) = 0 \end{aligned}$$

Use the following variable substitution

$$\begin{aligned}\Delta x_1 &= x_1 - x_1^0\\ \Delta x_2 &= x_2 - x_2^0\\ \Delta u &= u - u^0\end{aligned}$$

The linearized system is then

$$\begin{aligned}\begin{pmatrix}\Delta\dot{x}_1\\ \Delta\dot{x}_2\end{pmatrix} &= \begin{pmatrix}\frac{\partial f_1}{\partial x_1}(x_1^0,x_2^0,u^0) & \frac{\partial f_1}{\partial x_2}(x_1^0,x_2^0,u^0)\\ \frac{\partial f_2}{\partial x_1}(x_1^0,x_2^0,u^0) & \frac{\partial f_2}{\partial x_2}(x_1^0,x_2^0,u^0)\end{pmatrix}\begin{pmatrix}\Delta x_1\\ \Delta x_2\end{pmatrix} + \begin{pmatrix}\frac{\partial f_1}{\partial u}(x_1^0,x_2^0,u^0)\\ \frac{\partial f_2}{\partial u}(x_1^0,x_2^0,u^0)\end{pmatrix}\Delta u\\ \Delta y &= \begin{pmatrix}\frac{\partial g}{\partial x_1}(x_1^0,x_2^0,u^0) & \frac{\partial g}{\partial x_2}(x_1^0,x_2^0,u^0)\end{pmatrix}\begin{pmatrix}\Delta x_1\\ \Delta x_2\end{pmatrix} + \frac{\partial g}{\partial u}(x_1^0,x_2^0,u^0)\Delta u\end{aligned}$$

Where the derivates are given as their value in the stationary point. Using the specific values gives

$$\begin{aligned}\begin{pmatrix}\Delta\dot{x}_1\\ \Delta\dot{x}_2\end{pmatrix} &= \begin{pmatrix}0 & 1\\ -\frac{1}{2} & -1\end{pmatrix}\begin{pmatrix}\Delta x_1\\ \Delta x_2\end{pmatrix} + \begin{pmatrix}0\\ 2\end{pmatrix}\Delta u\\ \Delta y &= \begin{pmatrix}1 & 0\end{pmatrix}\begin{pmatrix}\Delta x_1\\ \Delta x_2\end{pmatrix}\end{aligned}$$

2.4 At the sought operating point it holds that

$$\begin{aligned}0 &= x_1^2 x_2 + 1\\ 0 &= x_1 x_2^2 + 1\\ y &= \arctan\frac{x_2}{x_1} + \frac{\pi^2}{8}\end{aligned}$$

which yields $x_1^0 = -1$, $x_2^0 = -1$ and $y^0 = \frac{\pi}{4} + \frac{\pi^2}{8}$. Computation of the partial derivatives now yields

$$\begin{aligned}&\frac{\partial f_1}{\partial x_1} = 2x_1x_2 && \frac{\partial f_1}{\partial x_2} = x_1^2 && \frac{\partial f_1}{\partial u} = \sqrt{2}\cos u\\ &\frac{\partial f_2}{\partial x_1} = x_2^2 && \frac{\partial f_2}{\partial x_2} = 2x_1x_2 && \frac{\partial f_2}{\partial u} = -\sqrt{2}\sin u\\ &\frac{\partial g}{\partial x_1} = \frac{-x_2}{x_1^2+x_2^2} && \frac{\partial g}{\partial x_2} = \frac{x_1}{x_1^2+x_2^2} && \frac{\partial g}{\partial u} = 4u\end{aligned}$$

With the variable substitution

$$\begin{aligned}\Delta u &= u - \frac{\pi}{4}\\ \Delta x_1 &= x_1 + 1\\ \Delta x_2 &= x_2 + 1\\ \Delta y &= y - \frac{\pi}{4} - \frac{\pi^2}{8}.\end{aligned}$$

the linearized system becomes

$$\begin{pmatrix} \dot{\Delta x_1} \\ \dot{\Delta x_2} \end{pmatrix} = \begin{pmatrix} 2 & 1 \\ 1 & 2 \end{pmatrix} \begin{pmatrix} \Delta x_1 \\ \Delta x_2 \end{pmatrix} + \begin{pmatrix} 1 \\ -1 \end{pmatrix} \Delta u$$
$$\Delta y = \begin{pmatrix} \frac{1}{2} & -\frac{1}{2} \end{pmatrix} \begin{pmatrix} \Delta x_1 \\ \Delta x_2 \end{pmatrix} + \pi \Delta u.$$

2.5 Blood Doping

The system dynamics are:

$$R(k) = (1-f) \cdot R(k-1) + r(k), \quad R(0) = R_{ref} \tag{2.1}$$
$$r(k) = 0.9 \cdot r(k-1) + u(k), \quad r(0) = f \cdot R_{ref} \tag{2.2}$$
$$u(k) = \begin{cases} 0.025 & \text{if } k = [1-19, 41-100] \\ 0.05 & \text{if } k = [21-40] \end{cases} \tag{2.3}$$

The matrices in the Simulink discrete state space block thus are:

$$A = \begin{bmatrix} (1-1/120) & 1 \\ 0 & 0.9 \end{bmatrix} \tag{2.4}$$
$$B = \begin{bmatrix} 0 \\ 1 \end{bmatrix} \tag{2.5}$$
$$C = \begin{bmatrix} 0 & 1 \\ 1 & 0 \end{bmatrix} \tag{2.6}$$
$$D = \begin{bmatrix} 0 \\ 0 \end{bmatrix} \tag{2.7}$$
$$\tag{2.8}$$

The initial conditions are:

$$x_0 = \begin{bmatrix} 0.25 \cdot 120 \\ 0.25 \end{bmatrix} \tag{2.9}$$

Define `epo` in the Matlab workspace as:

```
>> epo(:,1)= 1:100;
>> epo(:,2) = 0.025*ones(100,1);
>> epo(20:40,2)= 0.05;
```

2.6 The Simulink model can be seen in Fig. 2.1.

If α becomes large the bacteria outgrow the neuthrophiles and uncontrolled bacterial growth occurs.

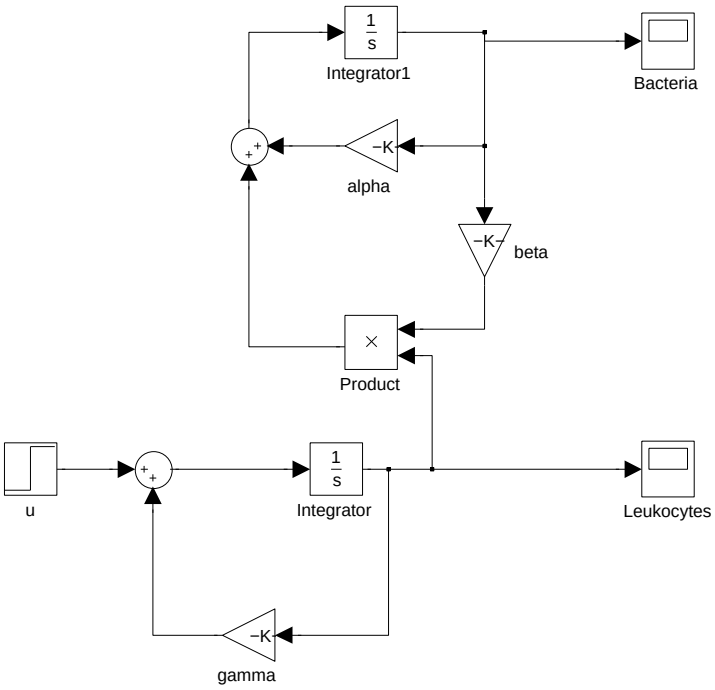


Figure 2.1 Simulink model for the Predator-Prey system

Solutions to Chapter 3. Control in Physiology 1

3.1 a. The transfer function is

$$\begin{aligned} G(s) &= C(sI-A)^{-1}B + D \\ &= \begin{pmatrix} -1 & 1 \end{pmatrix} \begin{pmatrix} s+2 & 0 \\ 0 & s+3 \end{pmatrix}^{-1} \begin{pmatrix} 5 \\ 2 \end{pmatrix} + 2 \\ &= \frac{2s^2+7s+1}{s^2+5s+6}. \end{aligned}$$

From the transfer function it is easy to determine the differential equation

$$\begin{aligned} Y(s) &= G(s)U(s) \\ (s^2+5s+6)Y(s) &= (2s^2+7s+1)U(s) \\ \ddot{y}+5\dot{y}+6y &= 2\ddot{u}+7\dot{u}+u \end{aligned}$$

b. The transfer function is

$$\begin{aligned} G(s) &= C(sI-A)^{-1}B + D \\ &= \begin{pmatrix} -2 & 1 \end{pmatrix} \begin{pmatrix} s+7 & -2 \\ 15 & s-4 \end{pmatrix}^{-1} \begin{pmatrix} 3 \\ 8 \end{pmatrix} = \\ &= \frac{2s+3}{s^2+3s+2}. \end{aligned}$$

The differential equation becomes

$$\begin{aligned} Y(s) &= G(s)U(s) \\ (s^2+3s+2)Y(s) &= (2s+3)U(s) \\ \ddot{y}+3\dot{y}+2y &= 2\dot{u}+3u \end{aligned}$$

3.2 a. Partial fraction expansion of the transfer function yields

$$G(s) = 2 + \frac{2}{s+3} - \frac{5}{s+2}$$

and by applying the inverse Laplace transform, one obtains the impulse response

$$h(t) = \mathcal{L}^{-1}G(s) = 2\delta(t) + 2e^{-3t} - 5e^{-2t}, \quad t \geq 0.$$

Comment. Because the system matrix was given in diagonal form, another possibility would have been to compute the impulse response as

$$h(t) = Ce^{At}B + D\delta(t) = \begin{pmatrix} -1 & 1 \end{pmatrix} \begin{pmatrix} e^{-2t} & 0 \\ 0 & e^{-3t} \end{pmatrix} \begin{pmatrix} 5 \\ 2 \end{pmatrix} + 2\delta(t), \quad t \geq 0.$$

The step response is computed by e.g. integrating the impulse response

$$\begin{aligned} y(t) &= \int_0^t h(\tau)d\tau = \int_0^t \left(2\delta(\tau) + 2e^{-3\tau} - 5e^{-2\tau}\right) d\tau \\ &= 2 + \left[\frac{5}{2}e^{-2\tau} - \frac{2}{3}e^{-3\tau}\right]_0^t \\ &= \frac{1}{6} + \frac{5}{2}e^{-2t} - \frac{2}{3}e^{-3t}, \quad t \geq 0. \end{aligned}$$

The step response can also be obtained by the inverse Laplace transform as follows

$$y(t) = \mathcal{L}^{-1}(G(s)\cdot\frac{1}{s}) = \mathcal{L}^{-1}\left(\frac{2}{s} + \frac{2}{s(s+3)} - \frac{5}{s(s+3)}\right) = \frac{1}{6} + \frac{5}{2}e^{-2t} - \frac{2}{3}e^{-3t}, \quad t \geq 0.$$

In MATLAB, the following code can be used

```
% Define the matrices
A = [-2 0 ; 0 -3];
B = [5;2];
C = [-1 1];
D = 2;

% Create the state space representation of the system
system = ss(A,B,C,D);

% Impulse response
impulse(system)

% Step response
step(system)
```

b. The transfer function has the partial fraction expansion

$$G(s) = \frac{1}{s+1} + \frac{1}{s+2}$$

and the impulse response becomes

$$h(t) = \mathcal{L}^{-1}G(s) = e^{-t} + e^{-2t}, \quad t \geq 0.$$

The step response is thus given by

$$y(t) = \int_0^t h(\tau)d\tau = \frac{3}{2} - e^{-t} - \frac{1}{2}e^{-2t}, \quad t \geq 0.$$

In MATLAB, the following code can be used

```
% Define the transfer function from the result in the previous exercise
s = tf('s'); % Determine frequency variable
G = (2*s+3)/(s^2+3*s+2);
```

```
% Impulse response
impulse(G)

% Step response
step(G)
```

3.3 After the Laplace transform, one obtains

$$\begin{aligned} sX &= AX + BU \\ Y &= CX + DU \end{aligned}$$

Solve for X

$$\begin{aligned} (sI - A)X &= BU \\ X &= (sI - A)^{-1}BU \end{aligned}$$

This gives

$$Y = C(sI - A)^{-1}BU + DU = \Big(C(sI - A)^{-1}B + D\Big)U$$

3.4 a. The poles are the solutions of the characteristic equation $s^2+4s+3 = 0$, i.e. $s = -1$ and $s = -3$. The system lacks zeros. The poles are in the left half-plane and the system is therefore stable.

b. The input (an impulse) has the Laplace transform $U(s) = 1$. The output becomes

$$Y(s) = G(s)U(s) = \frac{1}{s^2 + 4s + 3} = \frac{1}{(s+1)(s+3)}$$

Inverse Laplace transformation gives

$$h(t) = \frac{e^{-t} - e^{-3t}}{2}$$

The following code results in a plot of the impulse response:

```
s = tf('s');
G = 1/(s^2+4*s+3);
impulse(G)
```

3.5 To be (asymptotically) stable, all eigenvalues of the system matrix A must lie strictly within the left half plane (LHP). I.e. $\mathrm{Re}(\lambda_i) < 0$ $\forall\ i$.

The eigenvalues of A are given by the characteristic equation

$$\det(\lambda I - A) = 0$$

which in this case has two solutions, $\lambda_1 = -i$ and $\lambda_2 = i$. Since the eigenvalues do not lie strictly within the LHP, the system is not (asymptotically) stable.

3.6 a.

$$\begin{aligned} Y &= G_1(U + G_2 Y) \\ Y(1 - G_1 G_2) &= G_1 U \\ Y &= \frac{G_1}{1 - G_1 G_2} U \end{aligned}$$

b.

$$\begin{aligned} Y &= G_2(H_1 U + G_1 U + H_2 Y) \\ Y(1 - G_2 H_2) &= (G_2 H_1 + G_2 G_1) U \\ Y &= \frac{G_2 H_1 + G_2 G_1}{1 - G_2 H_2} U \end{aligned}$$

c. Introduce the auxiliary variable Z, being the output of G_1

$$\begin{aligned} Z &= G_1(U + G_3(Z + G_2 Z)) \\ Z(1 - G_1 G_3 - G_1 G_3 G_2) &= G_1 U \\ Z &= \frac{G_1}{1 - G_1 G_3 - G_1 G_3 G_2} U \\ Y &= \frac{G_2 G_1}{1 - G_1 G_3 - G_1 G_3 G_2} U \end{aligned}$$

3.7 a. The output is given by

$$y(t) = |G(3i)| \sin\Big(3t + \arg G(3i)\Big)$$

where

$$|G(i\omega)| = \frac{0.01\sqrt{1 + 100\omega^2}}{\sqrt{1 + \omega^2}\sqrt{1 + 0.01\omega^2}}$$

and

$$\arg G(i\omega) = \arctan 10\omega - \arctan \omega - \arctan 0.1\omega$$

For $\omega = 3$ one obtains $|G(i\omega)| = 0.0909$ and $\arg G(i\omega) = -0.003$ which gives

$$y(t) = 0.0909 \sin(3t - 0.003)$$

b. Reading from the plot yields $|G(3i)| \approx 0.09$ and $\arg G(3i) \approx 0$. We obtain

$$y(t) = 0.09 \sin 3t$$

Solutions to Chapter 4. Control in Physiology 2

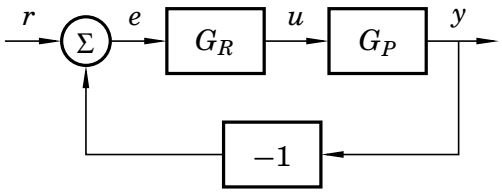
4.1 a. Laplace transformation of the differential equation yields

$$sY(s) + 0.01Y(s) = 0.01U(s)$$

The transfer function $G_P(s)$ is thus given by

$$Y(s) = G_P(s)U(s) = \frac{0.01}{s + 0.01}U(s)$$

b. The block diagram of the closed loop system becomes



The transfer function of the closed loop system becomes

$$G(s) = \frac{G_P(s)G_R(s)}{1 + G_P(s)G_R(s)}$$

c. $G_R(s) = K$, K is a constant, and the transfer function of the closed loop system becomes

$$G(s) = \frac{G_P(s)G_R(s)}{1 + G_P(s)G_R(s)} = \frac{\frac{0.01}{s+0.01}K}{1 + \frac{0.01}{s+0.01}K} = \frac{0.01K}{s + 0.01 + 0.01K}$$

d. The desired and actual characteristic polynomials are the same if all their coefficients match. Identification of coefficients yields

$$0.1 = 0.01 + 0.01K \quad \Leftrightarrow \quad K = 9$$

4.2 a. For the closed loop system it holds, when $R = 0$, that

$$U(s) = K(0 - Y(s)) = -K(G_P(s)U(s) + N(s))$$

from which one obtains

$$\begin{aligned} U(s) &= \frac{-K}{1 + KG_P(s)}N(s) \\ Y(s) &= G_P(s)U(s) + N(s) = \frac{1}{1 + KG_P(s)}N(s) \end{aligned} \tag{4.1}$$

b. Inserting $G_P(s) = \frac{1}{s+1}$ into (4.1) yields the relations

$$Y(s) = G_P(s)U(s) + N(s) = \frac{s+1}{s+1+K}N(s) =: G_{yn}(s)N(s)$$

In stationarity it holds that

$$\begin{aligned} y(t) &= A|G_{yn}(i\omega)|\sin(\omega t + \arg G_{yn}(i\omega)) \\ &= A\frac{\sqrt{1+\omega^2}}{\sqrt{(K+1)^2+\omega^2}}\sin\left(\omega t + \arctan\omega - \arctan\frac{\omega}{K+1}\right) \end{aligned}$$

c. With $A = 1$ and $K = 1$ the amplitudes of the oscillations

$$A = \sqrt{\frac{1+\omega^2}{4+\omega^2}}$$

For $\omega = 0.1$ rad/s the amplitude become

$$A \approx 0.5$$

while $\omega = 10$ rad/s yields

$$A \approx 1$$

4.3 a. The sensitivity function is given by

$$S(s) = \frac{1}{1+G_P(s)G_R(s)} = \frac{1}{1+\frac{6.5}{(s+1)^3}} = \frac{s^3+3s^2+3s+1}{s^3+3s^2+3s+7.5}$$

b. For $\omega = 0$ rad/s we have $|S(i\omega)| = 1/7.5$. Constant load disturbances are thus damped by a factor 7.5. The sensitivity functions has its maximum value $|S(i\omega)| \approx 10$ at $\omega \approx 1.6$ rad/s.

4.4 The closed loop system becomes

$$\begin{cases} \dot{x} = (A - BL)x + Bl_r r \\ y = Cx \end{cases}$$

The characteristic equation is thus

$$\det(sI - A + BL) = s^2 + (3 + l_1 + 2l_2)s + 2(1 + l_1 + l_2) = 0$$

We need $(s+4)^2 = s^2 + 8s + 16 = 0$. Identification of coefficients yields $l_1 = 9, \quad l_2 = -2$. The closed loop transfer function is $G(s) = C(sI - A + BL)^{-1}Bl_r$. The stationary gain is $G(0)$ is unity if

$$G(0) = C(-A + BL)^{-1}Bl_r = \frac{l_r}{4} = 1$$

yielding $l_r = 4$.

This type of controller can only be designed when the system is *controllable*. Information on *controllability* is given in the basic course in control.

Solutions to Chapter 5. Pharmacokinetics and Tracers

5.1 $C(t)$ is the concentration at time t. The initial condition and balance equation of the system are the following

$$C_0 = 300 \text{ [units/ml]}$$
$$\frac{dC}{dt} = -kC$$

The solution of the differential equation is

$$C(t) = C_0 e^{-kt}$$

After 8 days, the concentration is halved. Therefore, if the half-life is stated as $t_{1/2} = 8$, the concentration at $t_{1/2}$ is given by

$$C(t_{1/2}) = \frac{C_0}{2} = C_0 e^{-kt_{1/2}}$$

Thus k is,

$$k = \frac{\ln(2)}{t_{1/2}} = \frac{0.6931}{8} = 0.0866 \text{ days}^-1$$

Hence the formula for the concentration is given by

$$C(t) = C_0 e^{-0.0866 \cdot t} \text{ [units/ml]} \tag{5.1}$$

When $t = 7$ [days]

$$C(7) = C_0 e^{-0.0866 \cdot 7} = 163 \text{ [units/ml]}$$

Plot equation (5.1) using `MATLAB`

5.2 Use the same procedure as in exercise 5.1 to get k. Then use the following equation

$$\log(\frac{C_0}{0.4 \cdot C_0}) = \frac{k \cdot t}{2.3}$$

5.3 Use the same equation as in exercise 5.2. Set $t = 25$ [days] and $C_0/C = 90/80$ to determine k. Then determine $t_{1/2}$ by using the derived k and $\frac{C_0}{C} = 2$.

5.4 Sketch and discuss with your friend/TA.